



"Fra avfall til råvare" Extraction of metal products from MSWI fly ash

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4th Hydrometallurgy Seminar in Oslo



Norsep AS – owners and partners



- R&D and consultancy in process technology
- Developing world leading technology for water purification
- 9 employees (PhD, MSc, BSc) with diversified background in Porsgrunn and Molde, Norway
- Owners:
 - The founders 80%
 - AF Gruppen 20%



Waste treatment in Norway – opportunity for moving the boundaries for Circular economy?

Langøya 2013



- In Norway large amounts of hazardous waste has been safely landfilled at Langøya since the early 1990's
 - >300 000 tons of flyash (FA) from Scandinavia is annually neutralised with contaminated H_2SO_4 from industry to form gypsum
 - Heavy metals in FA and acid are stabilised and the risk for future leakage and contamination of the surroundings is minimised
 - The Langøya site is filled up by 2023
 - State-of-the-art solutions for waste treatment as of the 1990's may be challenged
- Potential for new technology to move the boundaries for circular economy, significantly reducing the volumes for landfill
 - Valuable materials in the waste streams are lost
 - Metal recovery from fly ash implemented in Switzerland
 - Development projects in Sweden/Denmark
 - Activities also in Japan.

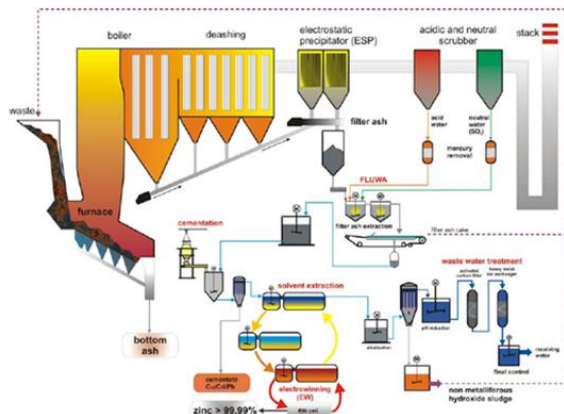
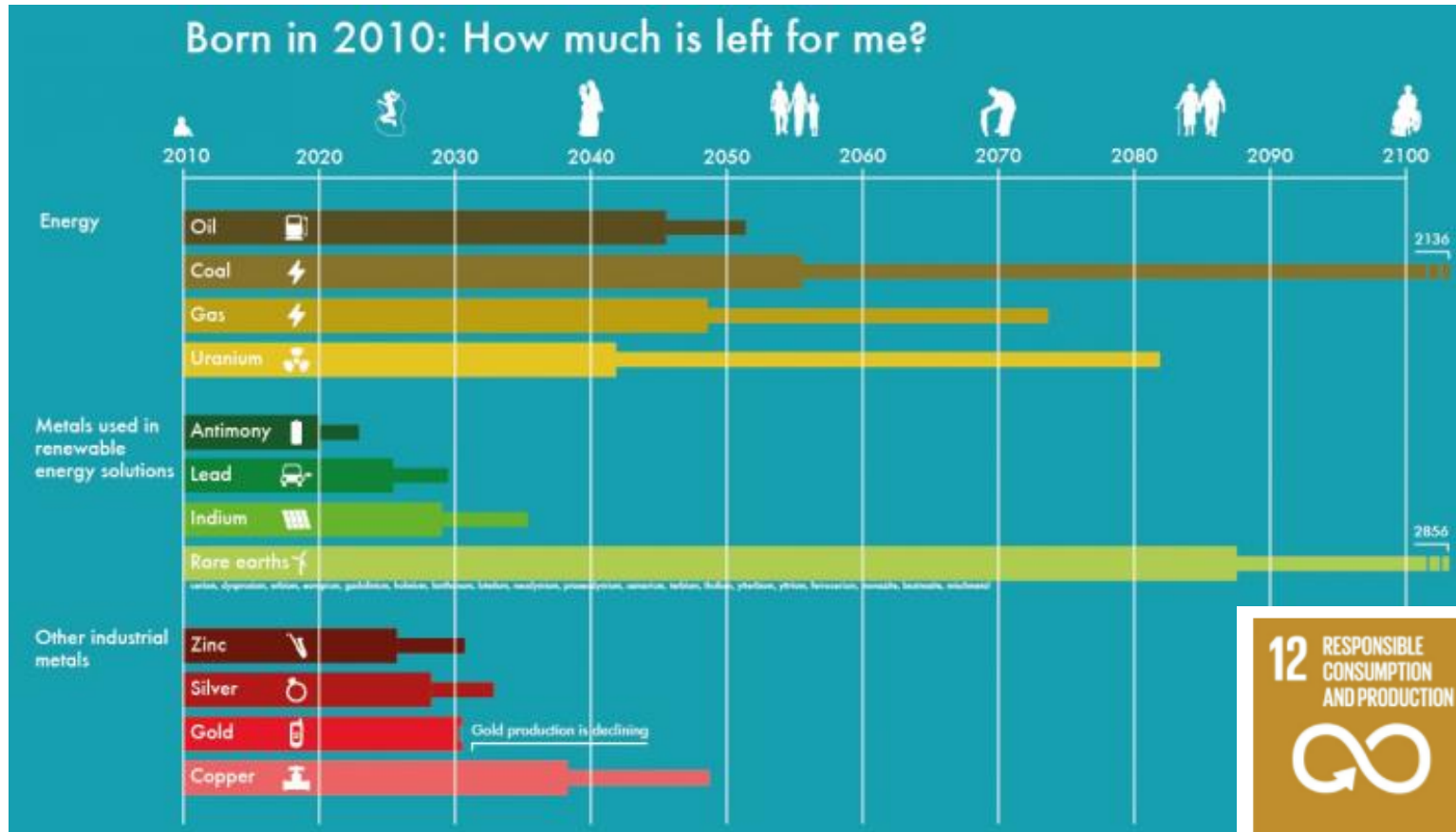


Figure 7. Process diagram for waste incineration with sustainable residues management and recovery of recyclable materials (FLUREC)

Sources: Vurdering av deponeringskapasitet for farlig avfall, Miljødirektoratet 2015; <http://www.noah.no/samfunnsansvar/deponiovervaking-langoya/> ; Avfall Norge, Potensialet for økt materialgjenvinning av farlig avfall i Norge, Rapport nr.: 02/2017, 13.01.2017; http://www.recydepotech.at/media/2.3_Weibel_1.pdf ; http://ec.europa.eu/environment/life/project/Projects/index.cfm?fuseaction=search.dspPage&n_proj_id=5787; JP2005272955(A), 2005 (Dowa Mining); JP2007186761(A), 2007; Mitsui Mining;

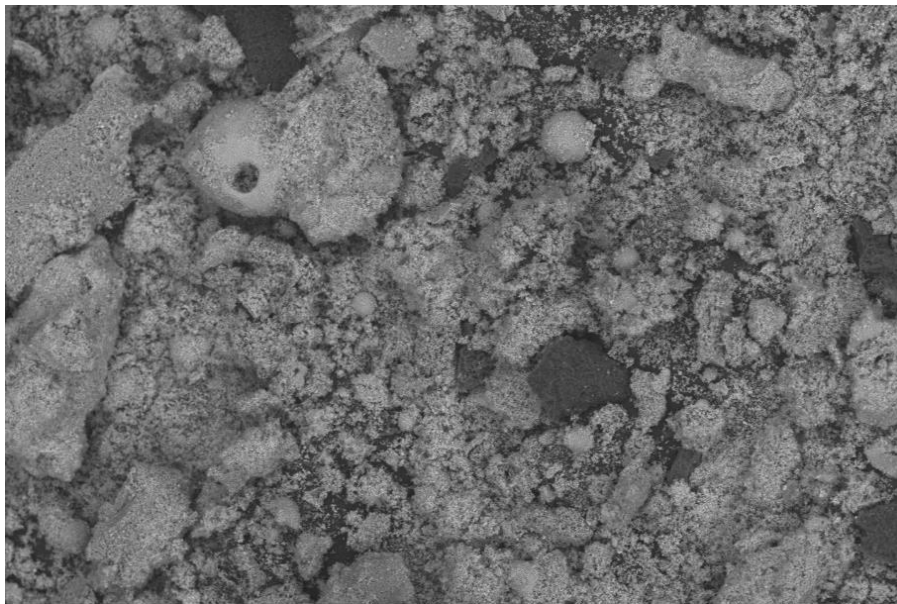
Fly ash contains non-renewable resources the world can run out of within the next generation



Zinc

- Estimated *reserves* in traditional ores ~220 mill tons
- Annual consumption 13.1 mill tons (2010-2014 average)
- Current recycling rate 31%
- ~25 years until depletion of natural Zn reserves
- Despite this, Zn is *not* on EU's Critical Raw Materials list.

Analyses av fly ash – Sample from EGE Haraldrud, Oslo



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Prove merket:		<i>Semikvantitativ XRF-analyse</i>
Flyveaske		
Parameter	Enhet	
Ca, Kalsium	%	23
Cl, Klor	%	18
Na, Natrium	%	10
K, Kalium	%	7
S, Svovel	%	4
Si, Silisium	%	2,6
Al, Aluminium	%	1,9
Ti, Titan	%	1,5
P, Fosfor	%	1,0
Br, Brom	%	0,2

Prøve merket: Flyveaske		<i>*Oppslutning i mikrobølgeovn</i>	<i>Grenseverdi farlig avfall</i>
Parameter	Enhet		
As, Arsen	mg/kg	35	1 000**
Cd, Kadmium	mg/kg	79	1 000**
Cr, Krom	mg/kg	300	1 000****
Cu, Kobber	mg/kg	640	2 500**
Hg, Kvikksølv	mg/kg	19	1 000***
Ni, Nikkel	mg/kg	53	1 000**
Pb, Bly	mg/kg	1000	2 500***
Zn, Sink	mg/kg	11000	2 500**

*Etter oppslutning og analyse med ICP-AES. Bestemmelse av Hg bestemt ved CV-AAS

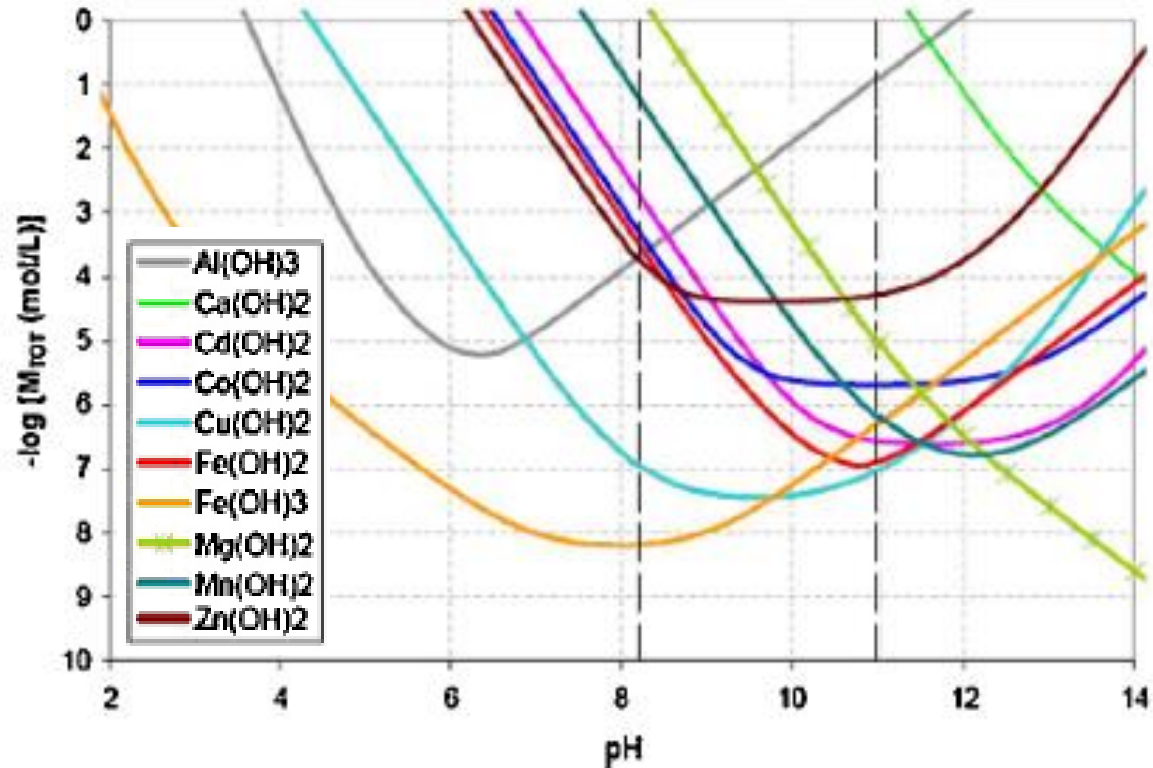
**Grenseverdier for oksider av parameter i den europeiske stofflisten.

***Grenseverdier for kvikksølvforbindelser og blyforbindelser i den europeiske stoffli.

****Grenseverdi for kromat i den europeiske stofflisten.



Fly ash partly dissolves in strong acids - metals in solution precipitate as hydroxides with increasing pH



Solubility of metal hydroxides increases with decreasing pH. Most metal hydroxides have minimum solubility in the pH range 6-11

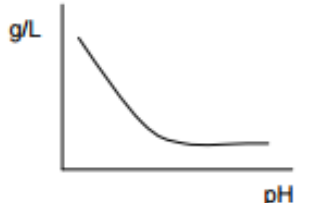


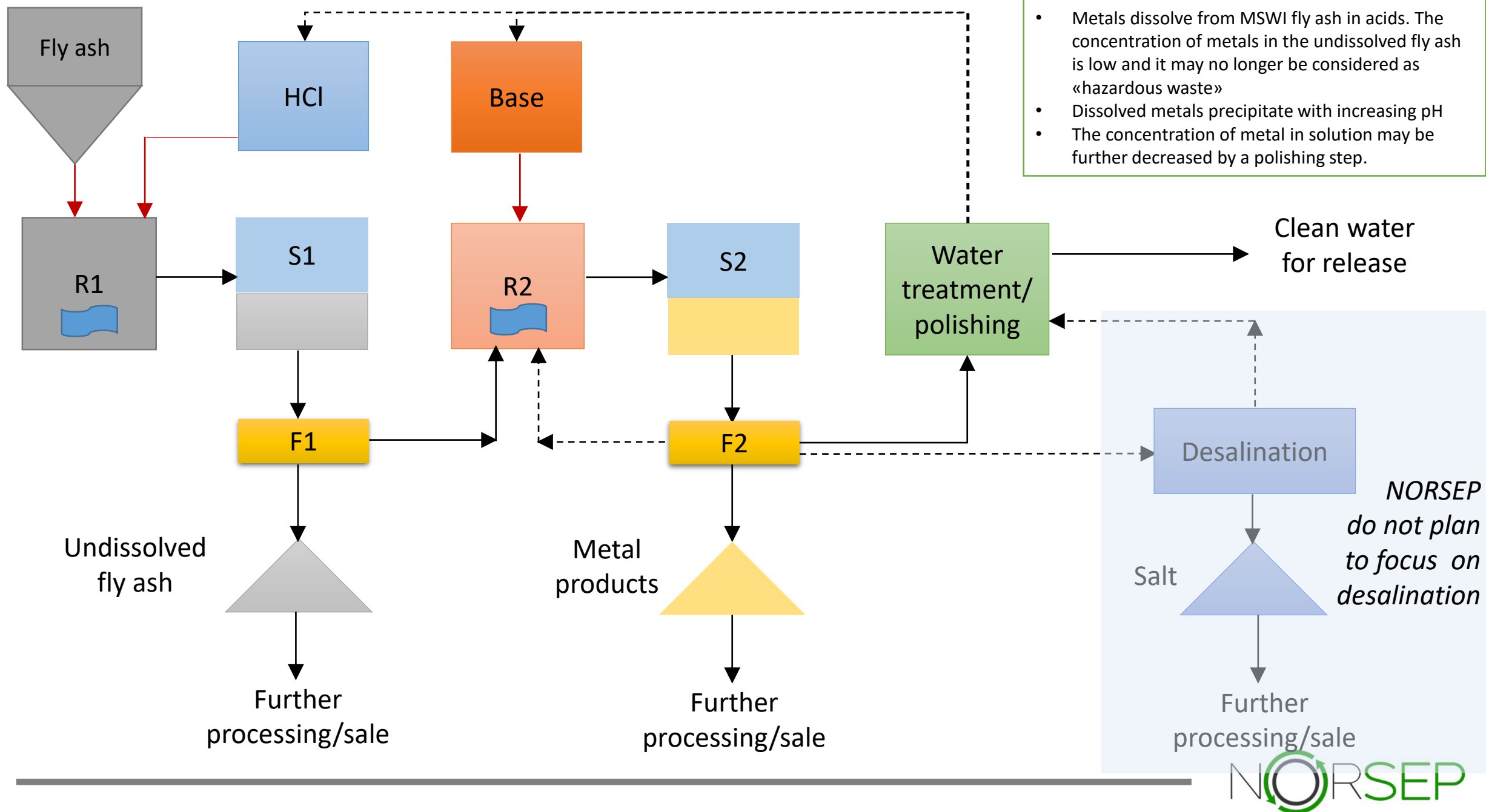
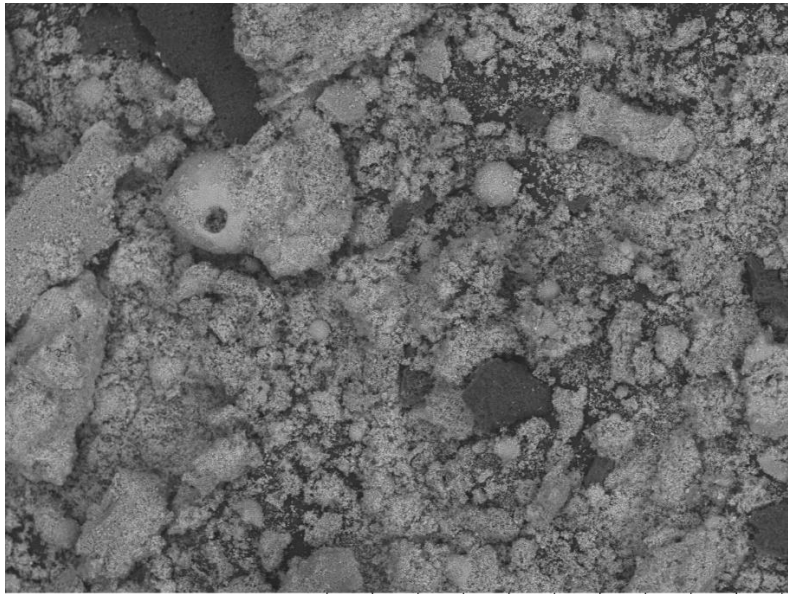
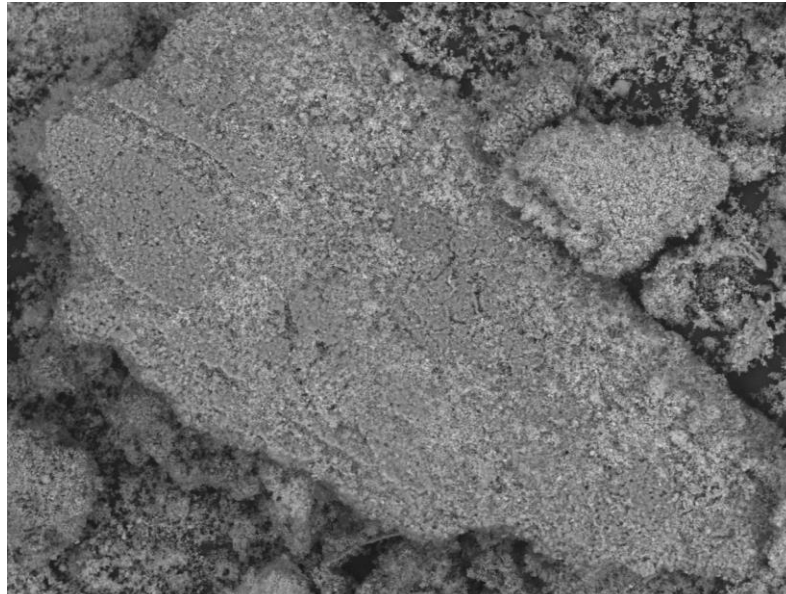
Species	Metals	Leachability vs. pH
Cation-forming and non-amphoteric elements Leaching is approximately constant at pH > 8	Ca	
Amphoteric elements Minimum leaching around pH 7	Al, Cd, Co, Cu, Ni, Pb, Zn	
Oxyanion-forming elements Leaching decreases at pH > 10	As, B, Cr, Mn, Mo, Sb, V	

Figure 3.3. The influence of pH on the leaching of certain metals from MSWI ashes.

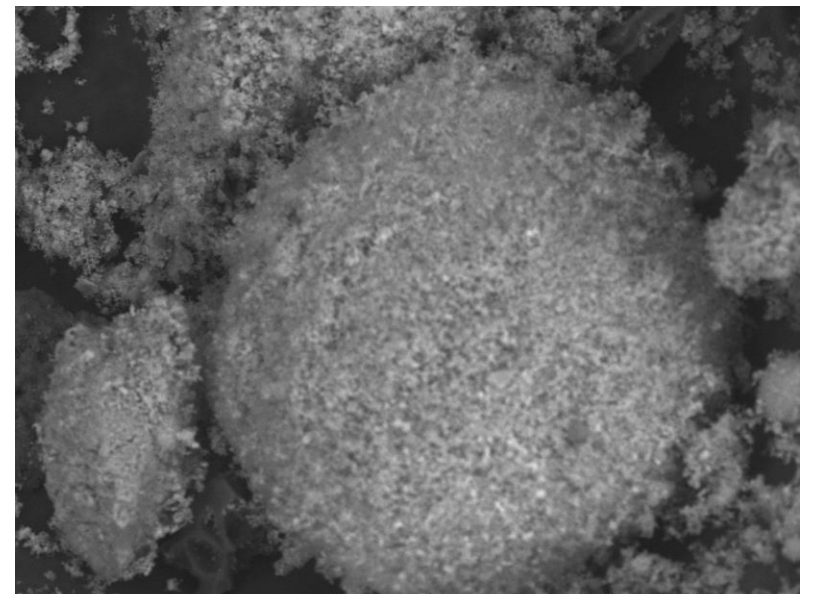




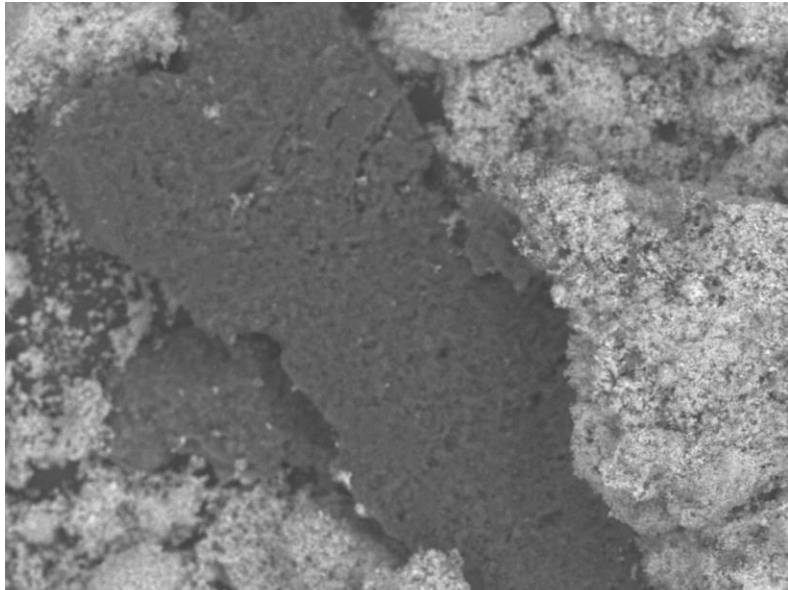
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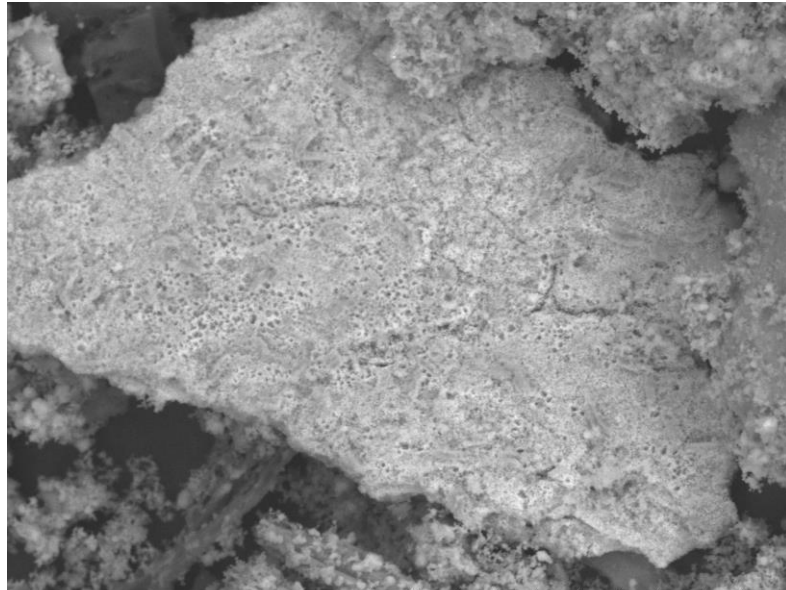
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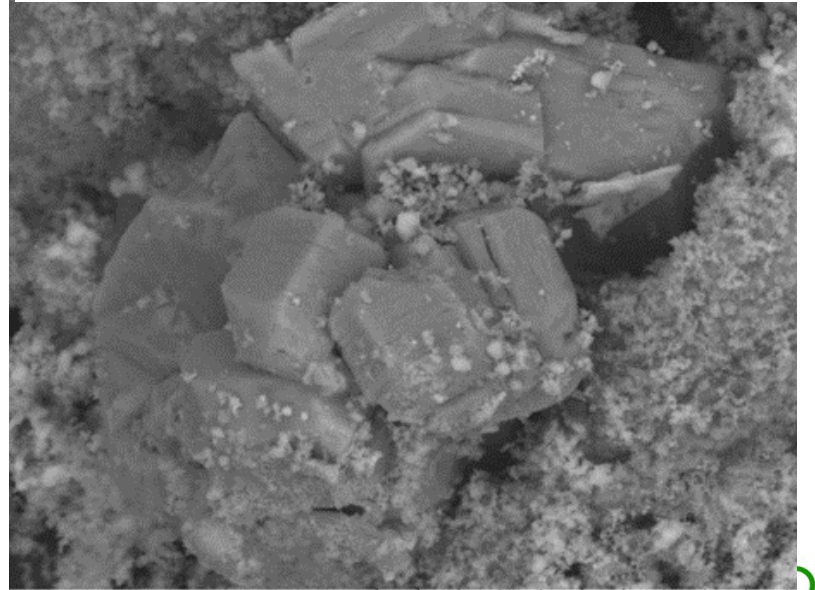
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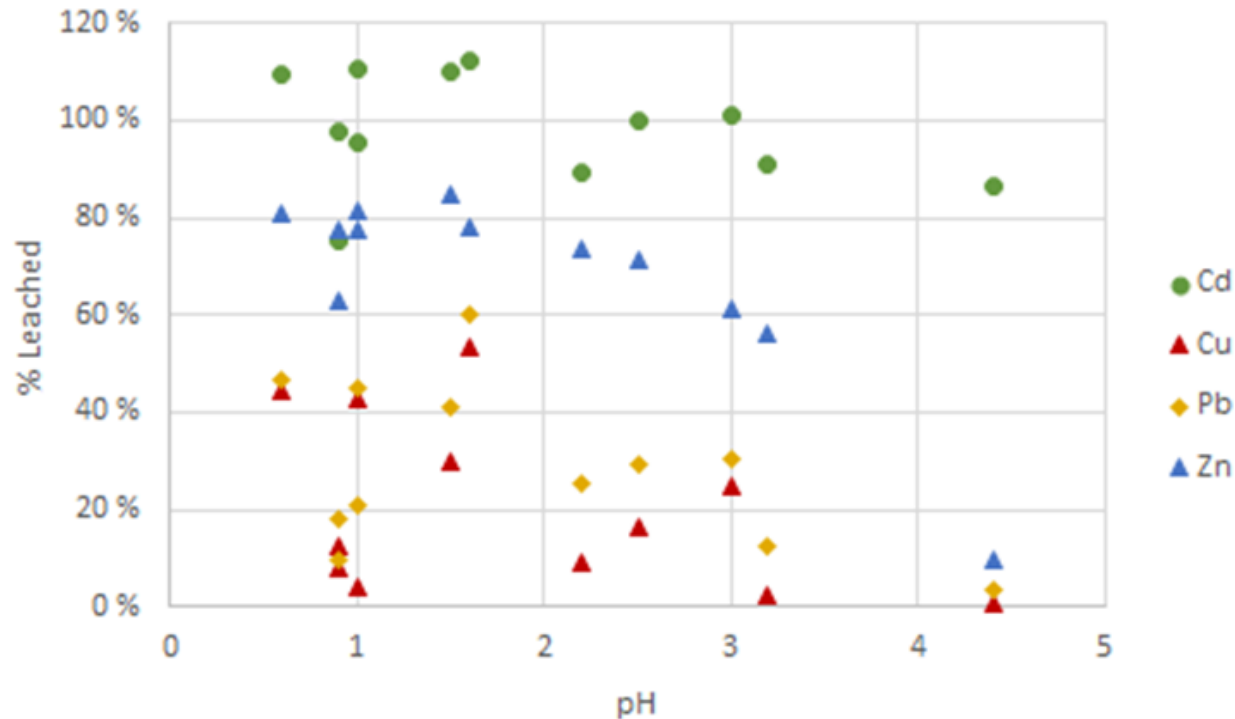


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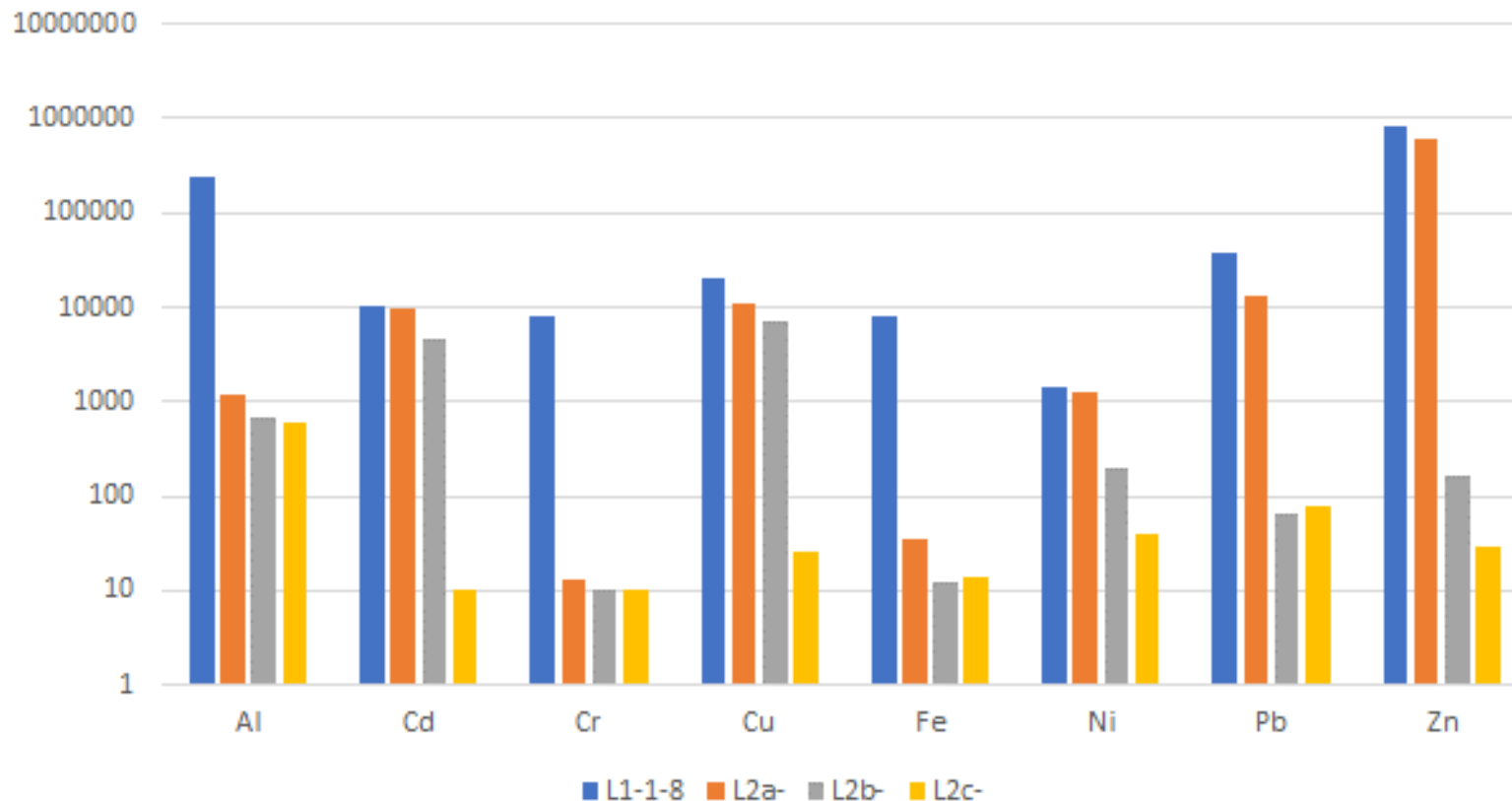
Leaching, $C_0=1M$



- % leached decreases with increasing pH
- 75% Zn dissolves even at pH = 2.5
- Cd dissolves 100% also at relatively high pH
- Pb and Cu dissolves <50%, inconsistent results.

- At low pH several of the compounds in the fly ash dissolve, causing pH to increase
 - The stronger the acid is initially, the more compounds dissolve
- When more fly ash is added, some compounds still dissolve, while other compounds that dissolved at the lower pH no longer dissolve
- At the same time some phases (hydroxides), may start to precipitate
 - At a certain pH range dissolution of some compounds and precipitation of others may occur simultaneously
- At higher pH dissolution ceases and precipitation dominates.

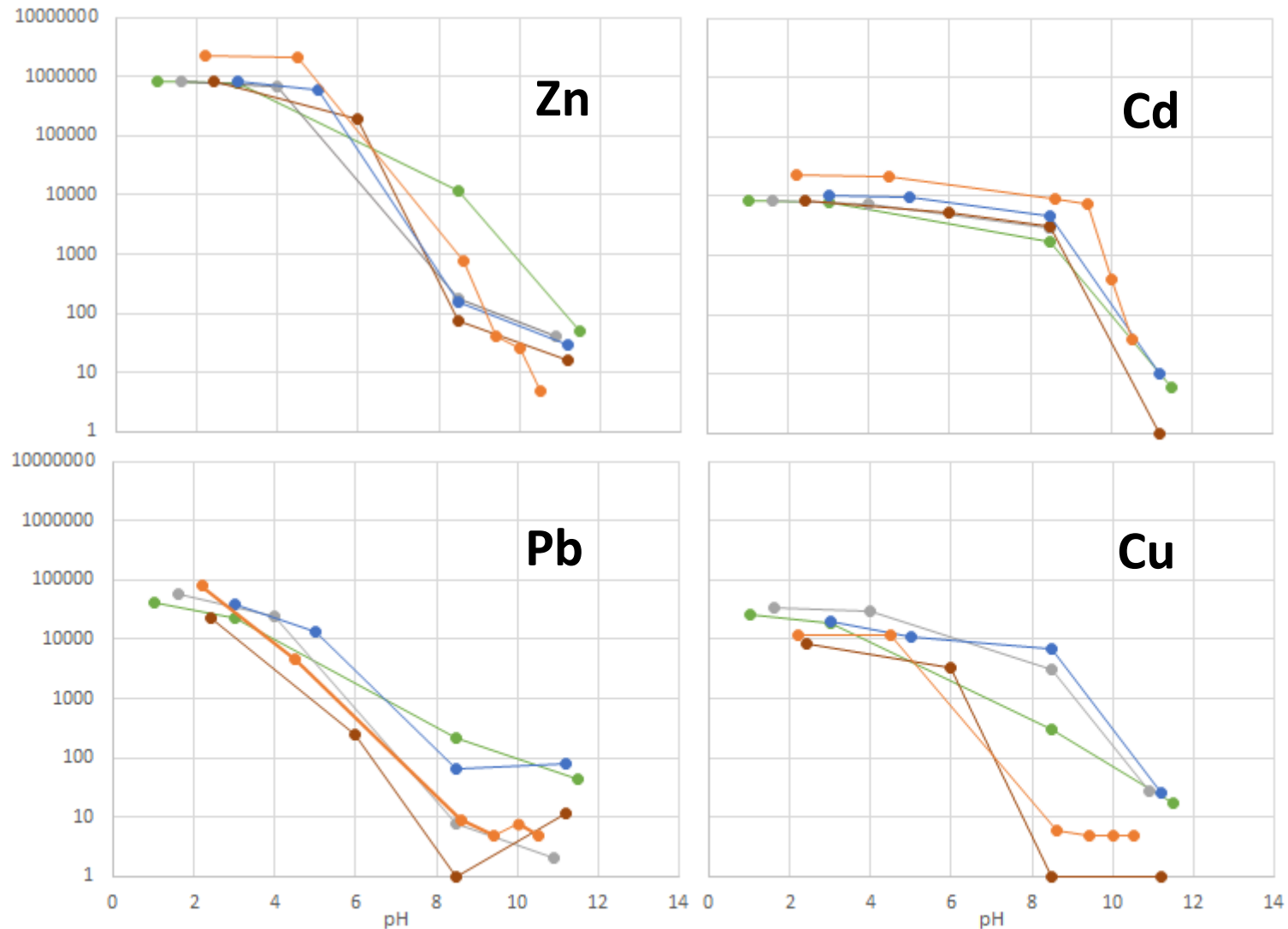
Precipitation – dissolved elements can partly be separated in different fractions



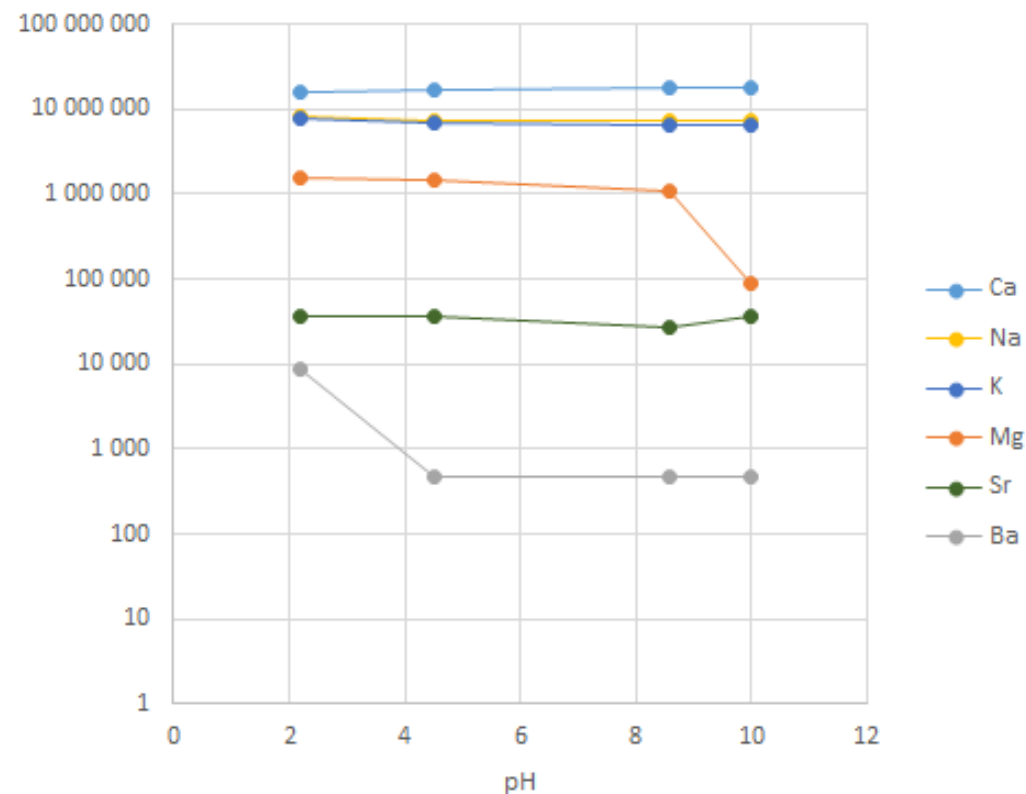
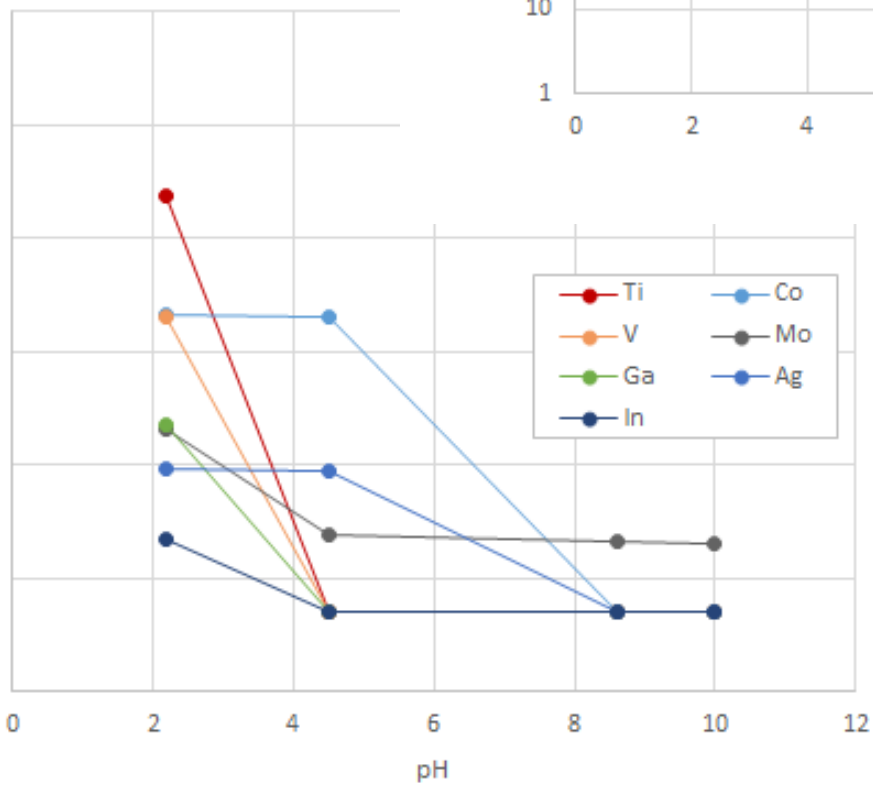
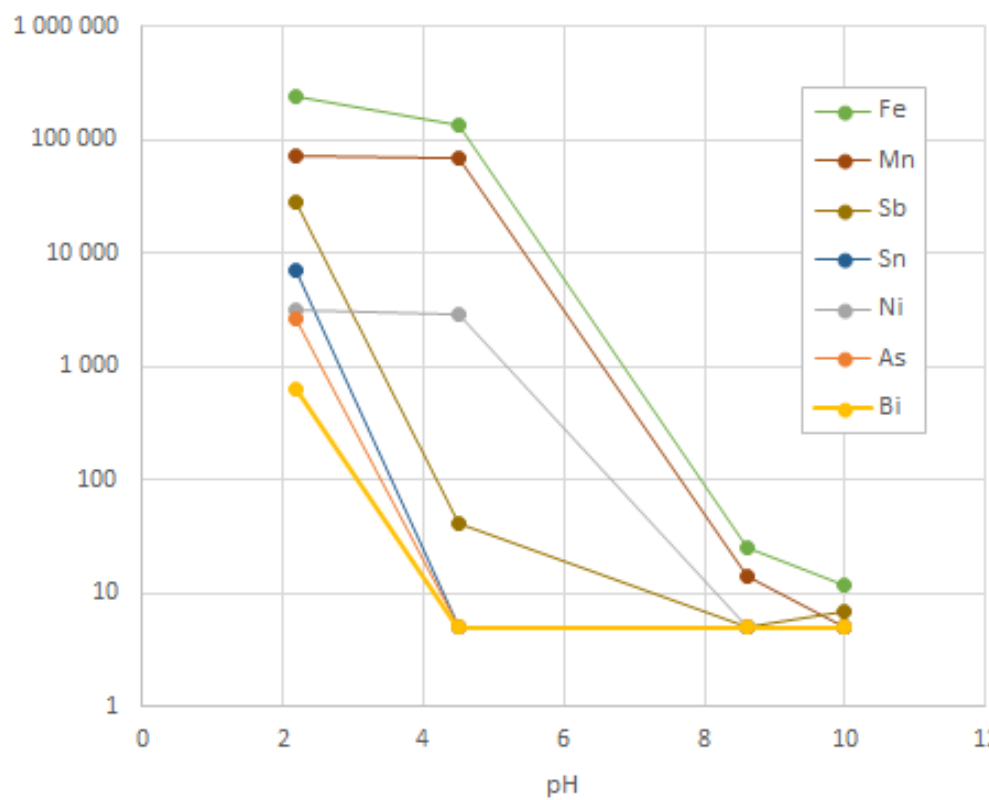
- $\text{pH}(\text{L1}) < \text{pH}(\text{a}) < \text{pH}(\text{b}) < \text{pH}(\text{c})$
- Al, Fe og Cr precipitate mainly before pH level a
- Zn (and Pb) precipitates between pH levels a and b
- Cd (and Cu) mainly precipitates between pH levels b and c

A Zn enriched metal product can be prepared by extracting precipitates at appropriate pH levels.

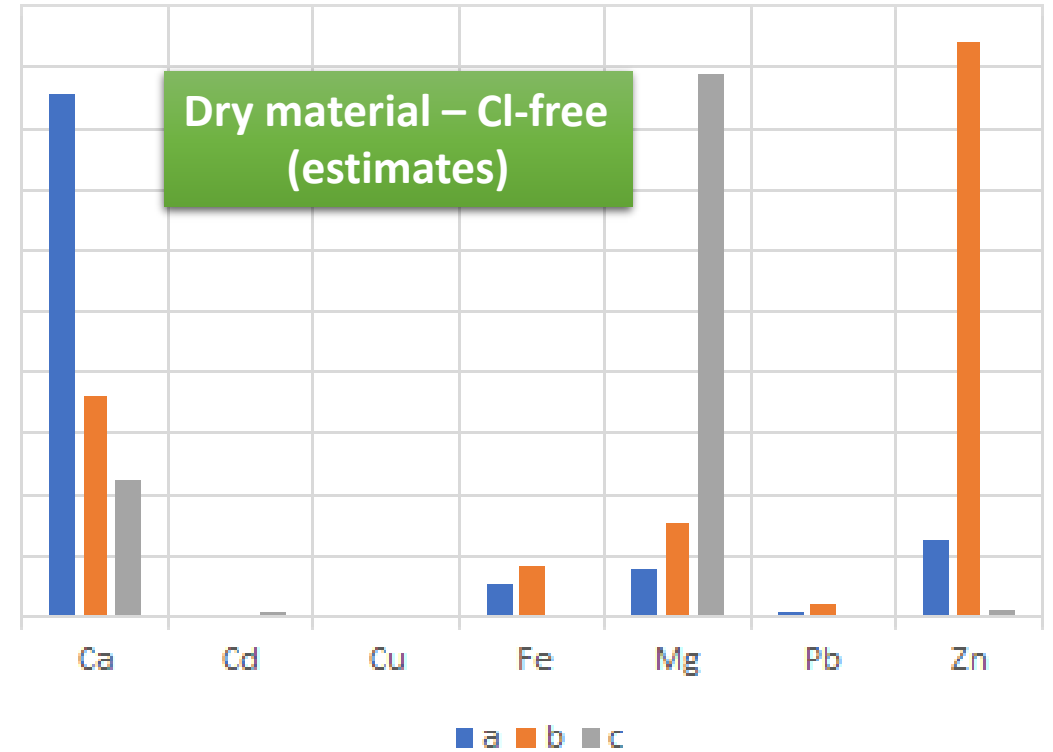
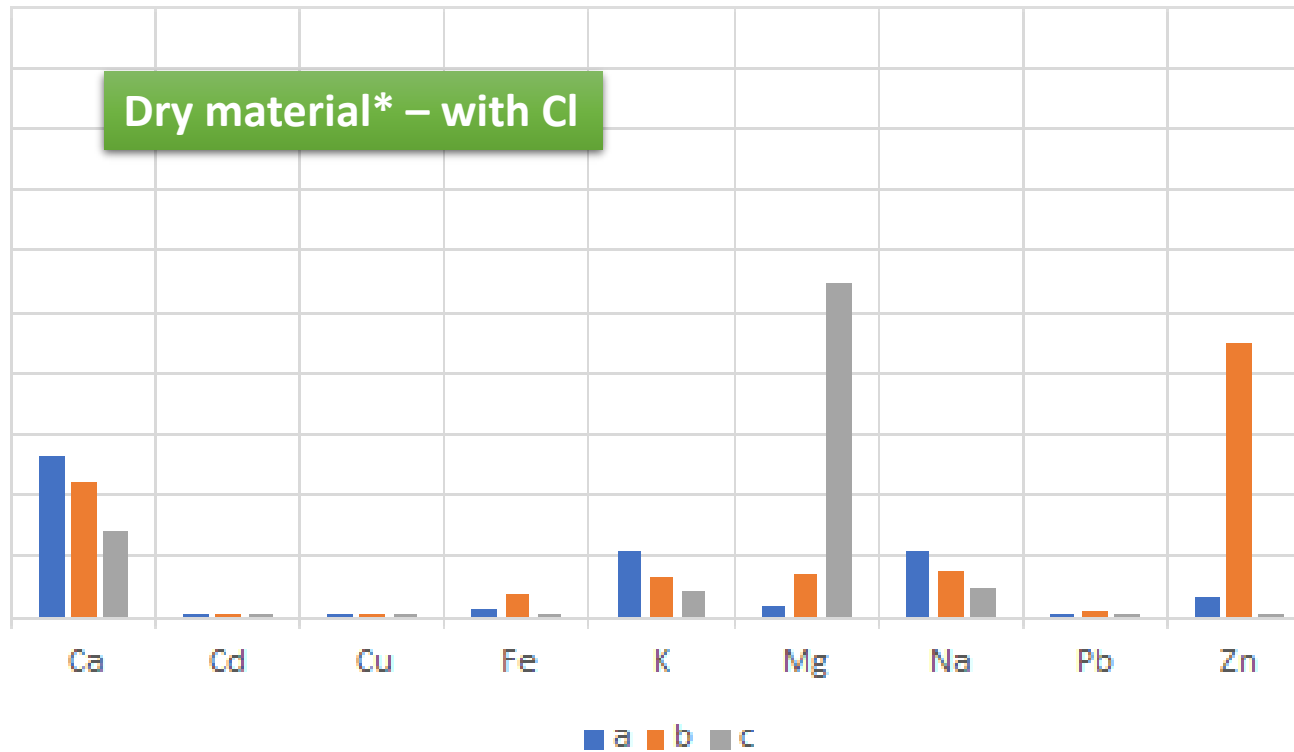
Precipitation vs. pH: Zn, Pb – Cd, Cu



Precipitation vs. pH – other elements

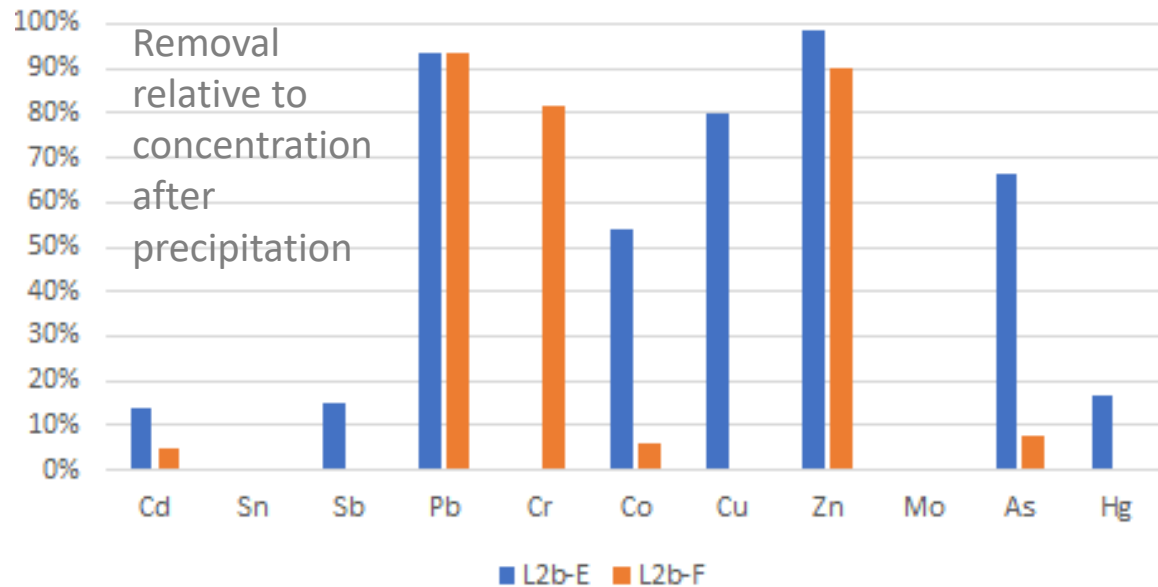


Precipitated materials

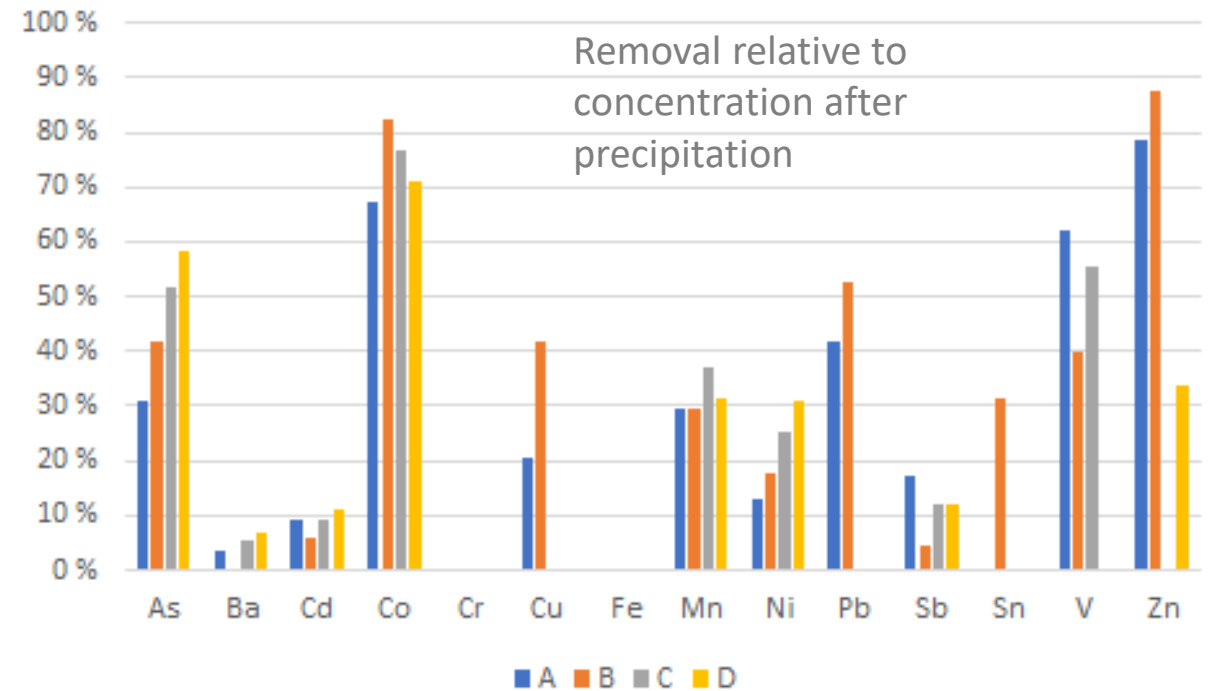


* Drying at 105°C. Chlorides in moisture precipitates during evaporation and contaminate the surfaces.

Polishing of NORSEP wastewater using different adsorbents (A-F)



- Different adsorbents (E and F) can selectively decrease the metal contents significantly
- Additional removal of >90% have been demonstrated for Pb and Zn, approx. 80% for Cr and Cu, and 50-70% for Co and As
- Adsorption of Co, Sb and Mo is limited for the adsorbents tested.



- Different adsorbents (A, B, C and D) can selectively decrease the metal contents significantly
- From the solution with pH adjusted to level b, additional removal of 70-90% have been demonstrated for Co and Zn, and above 50% for As, Pb and V
- Ba, Cd, Mn, Ni and Sb exhibit limited response to adsorption, at least for the adsorbents A-D tested.

Phase 2 of NORSEP project - ongoing

- Lab-activities
 - Verify process – create interest
 - Input for design of pilot
 - Prepare test material for evaluation of process equipment
- Pilot - preparations
 - F-park Herøya – June 2018
 - Equipment
- Application for EU-funding phase 3 for building of a demonstration facility at a WtE -plant
 - Prepare and submit application – deadline May 2018
 - Professional assistance in the application process



A compact NORSEP -facility



- Retrofit
- New build

Compact fly ash treatment facilities at existing or new MSWI sites

- Utilise acid already available from wet scrubbers
- May utilise existing water treatment system
- Less variation in fly ash composition
- Infrastructure for energy recovery in place.

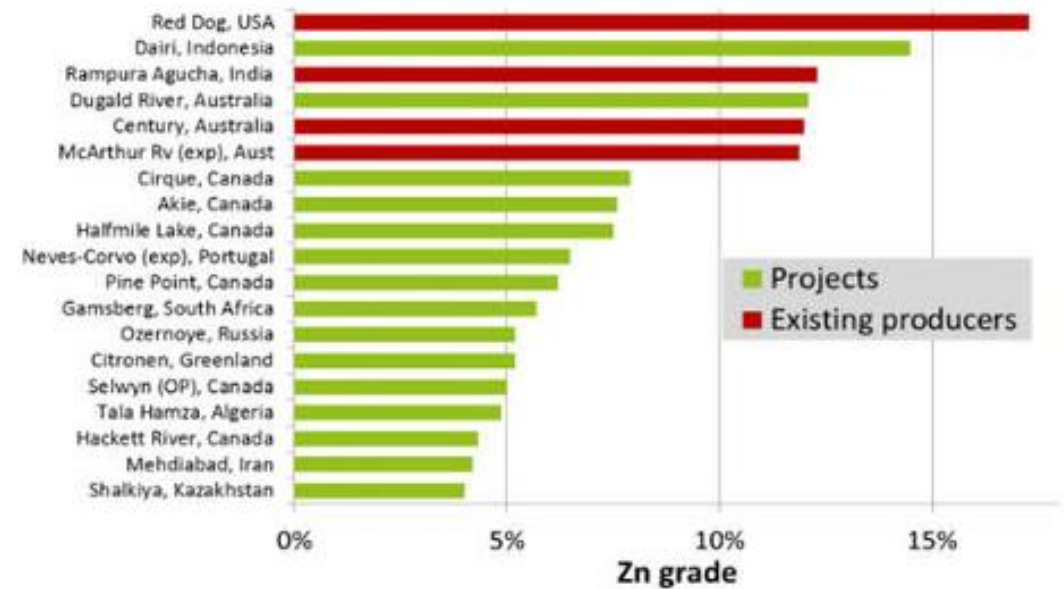
Centralised plants, e.g. at the sites of companies utilising main material streams.

- CAPEX/ton

Urban Mining from fly ash becomes competitive ?

- One or more material streams from NORSEP-process will mainly consist of metal hydroxides
- With Zn content of 20-50% the metal hydroxide concentrate(s) could be tailored to become commercially attractive for subsequent production of oxides and/or extraction of metals
 - Mining projects with zinc grades of 4% are considered for realisation

Example: 300.000 tons of FA containing ~1.5% Zn may yield 4500 tons of Zn, representing ~10 mill €



LME ZINC HISTORICAL PRICES GRAPH



NORSEP – materials produced from waste streams



*Haraldrud MSWI plant, Oslo, Norway.
Capacity 100000 tons/yr.*

- Raw materials
 - Flyash
 - Waste acid
 - Waste base
- Products
 - Undissolved flyash
 - Metal concentrates
 - (Salts)

Commercially attractive products may be prepared from a combination of waste streams, with minimum use of virgin raw materials

