



NIKKELVERK  
A GLENCORE COMPANY

Hydromet-seminar at IFE, March 2017

**The Nickel Laterite Industry with a Focus on Hydrometallurgy**  
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# Nickel industry in perspective...



- Natural resource-industries (peak production in mln tonnes per year):

|                |       |
|----------------|-------|
| – Coal:        | 8 200 |
| – Limestone:   | 5 000 |
| – Crude Oil:   | 4 000 |
| – Natural Gas: | 2 600 |
| – Grains:      | 2 500 |
| – Iron ore:    | 2 300 |
| – Steel:       | 1 700 |
| – S/S-equiv.:  | 70    |
| – Al:          | 60    |
| – Cu:          | 20    |
| – Zn:          | 13    |
| – Pb:          | 4.7   |
| – Ni:          | 2.0   |
| – Co:          | 0.1   |

China consumes ~40-50% of many of these commodities, except grains, crude oil, natural gas and S/H<sub>2</sub>SO<sub>4</sub>.

But the price picture is inverse, Ni is ~200 times more expensive than coal...

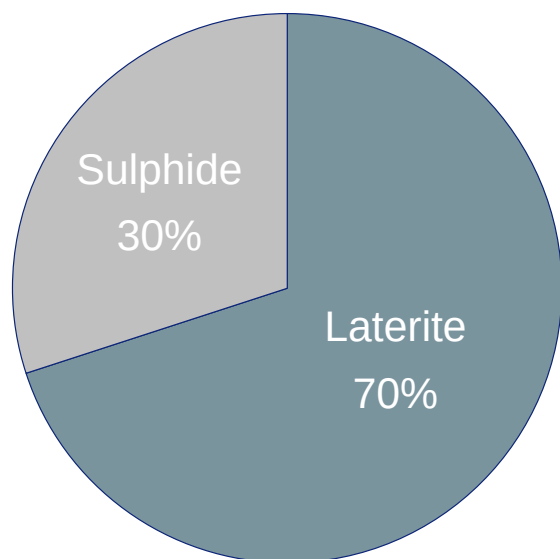


# Global nickel laterite resources

(Source, G.W.Bacon, Inco 2004)

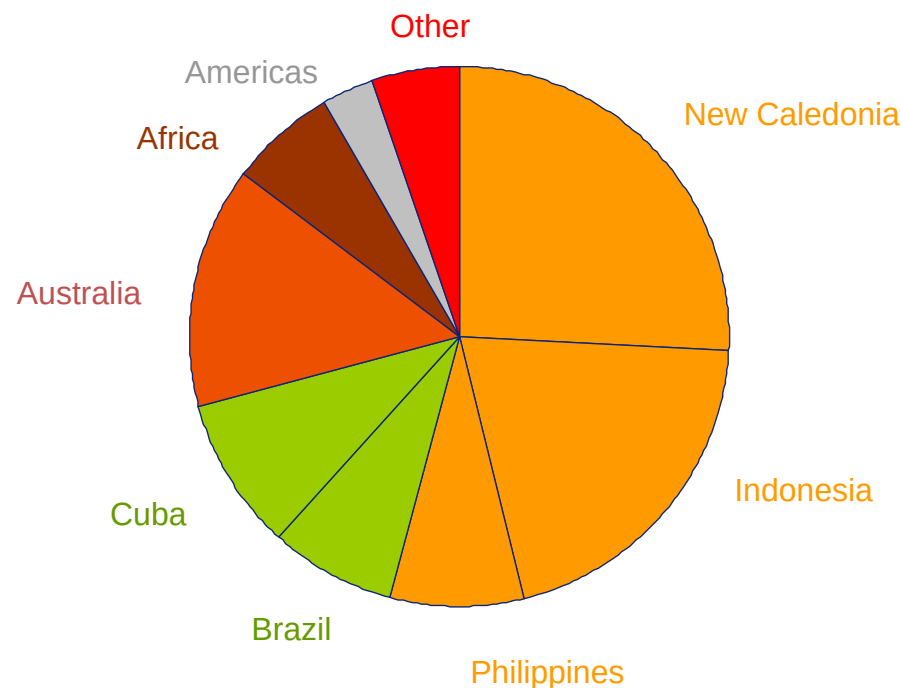


Global Nickel Resources  
230 Mt Contained Nickel



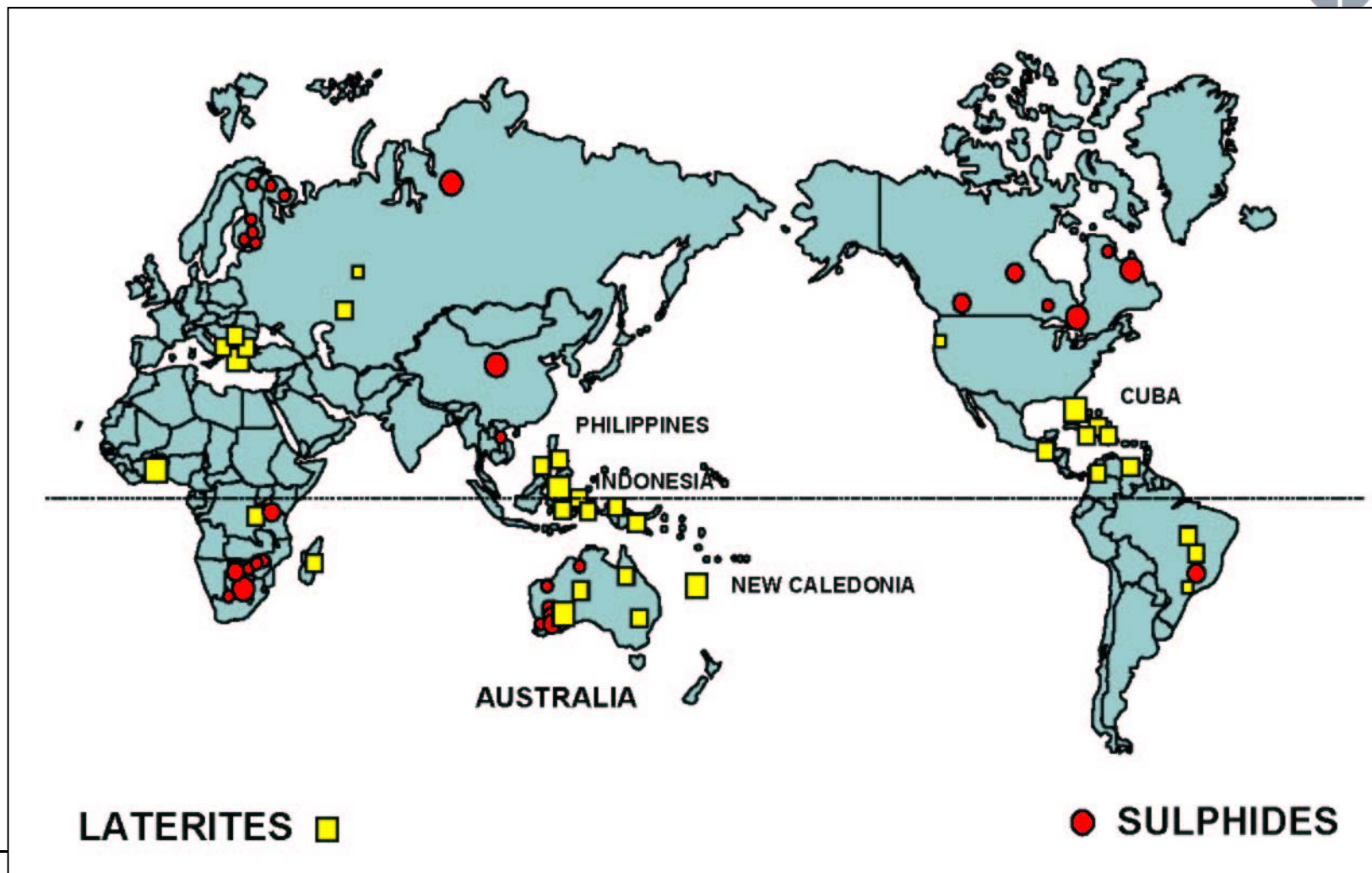
$R/P = 230/2.3 \sim 100 \text{ yrs}$

Laterite Resources by Region  
161 Mt Contained Nickel



Apparantly no lack of resources...

# Distribution of global nickel resources



# Typical profile for laterite ore, applicable technology

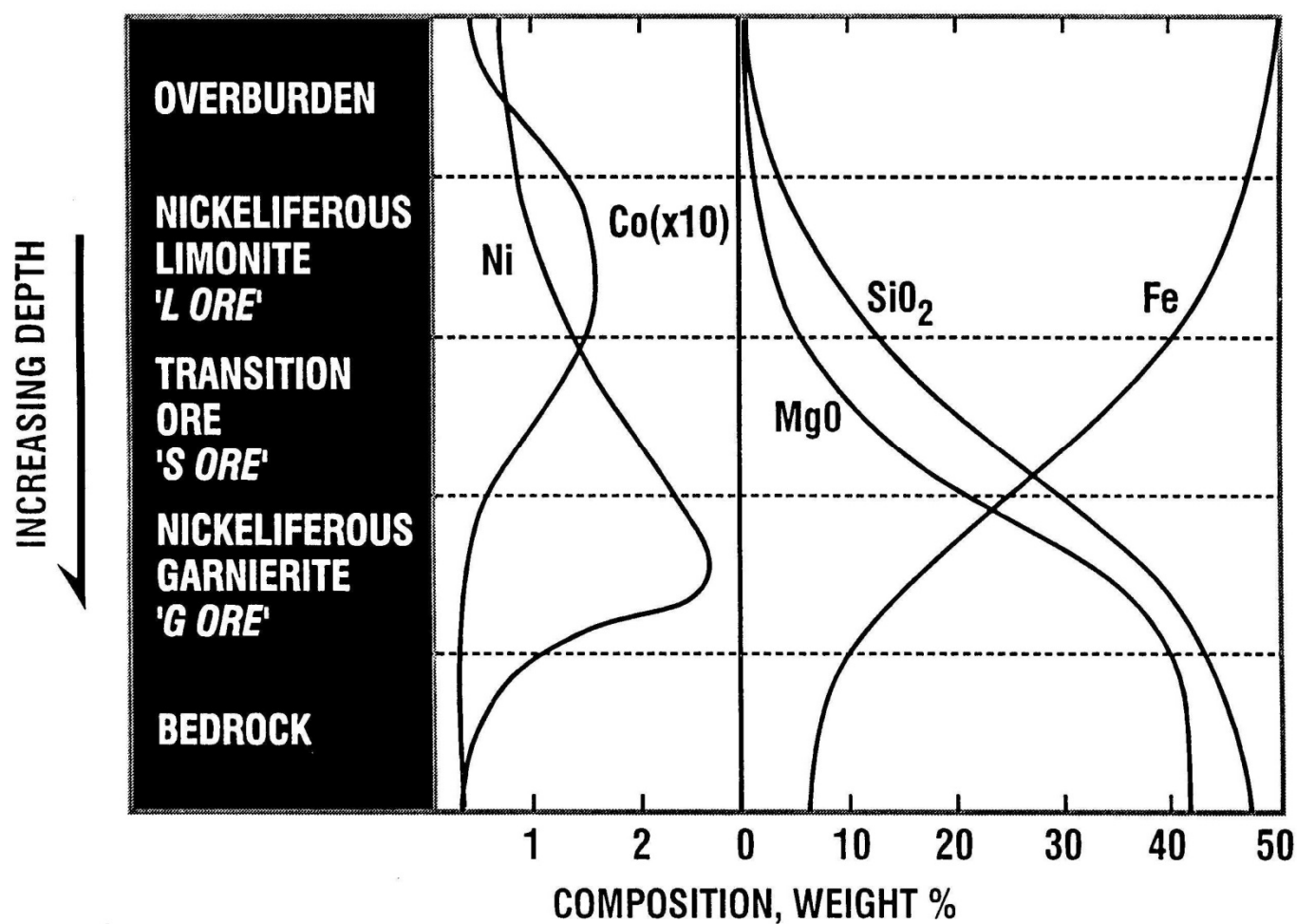


| Idealized Laterite     | Approximate Analysis (%) |              |              |                                |              |                  | Extractive Procedure              |
|------------------------|--------------------------|--------------|--------------|--------------------------------|--------------|------------------|-----------------------------------|
|                        | Ni                       | Co           | Fe           | Cr <sub>2</sub> O <sub>3</sub> | MgO          | SiO <sub>2</sub> |                                   |
| Hematitic Cap          | <0.8                     | <0.1         | >50.0        | >1.0                           | <0.5         |                  | Overburden to Stockpile           |
| Nickeliferous Limonite | 0.8 to 1.5               | 0.1 to 0.2   | 40.0 to 50.0 | 2.0 to 5.0                     | 0.5 to 5.0   | 0 to 10.0        | Hydrometallurgy                   |
| Altered Peridotite     | 1.5 to 1.8               | 0.02 to 0.1  | 25.0 to 40.0 | 1.0 to 2.0                     | 5.0 to 15.0  | 10.0 to 30.0     | Hydrometallurgy to Pyrometallurgy |
|                        | 1.8 to 3.0               |              | 10.0 to 25.0 |                                | 15.0 to 35.0 | 30.0 to 50.0     | Pyrometallurgy                    |
| Unaltered Peridotite   | 0.25                     | 0.01 to 0.02 | 5.0          | 0.2 to 1.0                     | 35.0 to 45.0 |                  | Left In-Situ                      |

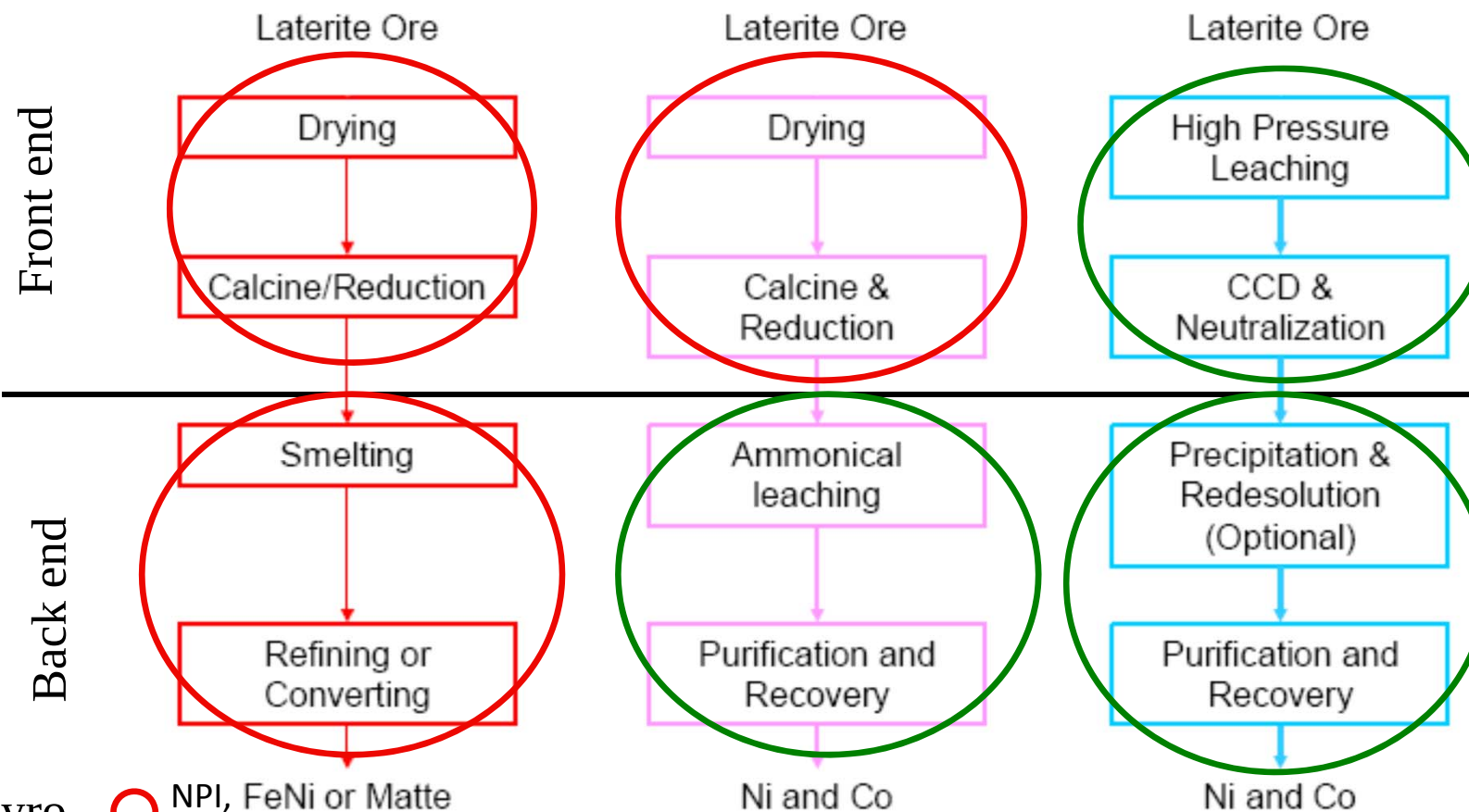
"Peridotite" = Mineral class  $(X_a, Y_b)SiO_4$ , or  $XO(Y_c, Z_d)SiO_4$ , example. olivine,  $X=Mg$



# Illustrated with concentration profiles



# Laterite Nickel Production - Principal Technologies



Pyro  
Hydro



NPI, FeNi or Matte

**Smelting**

**Caron Process**

**HPAL**

# Disadvantage for laterites vs. sulphide nickel ores

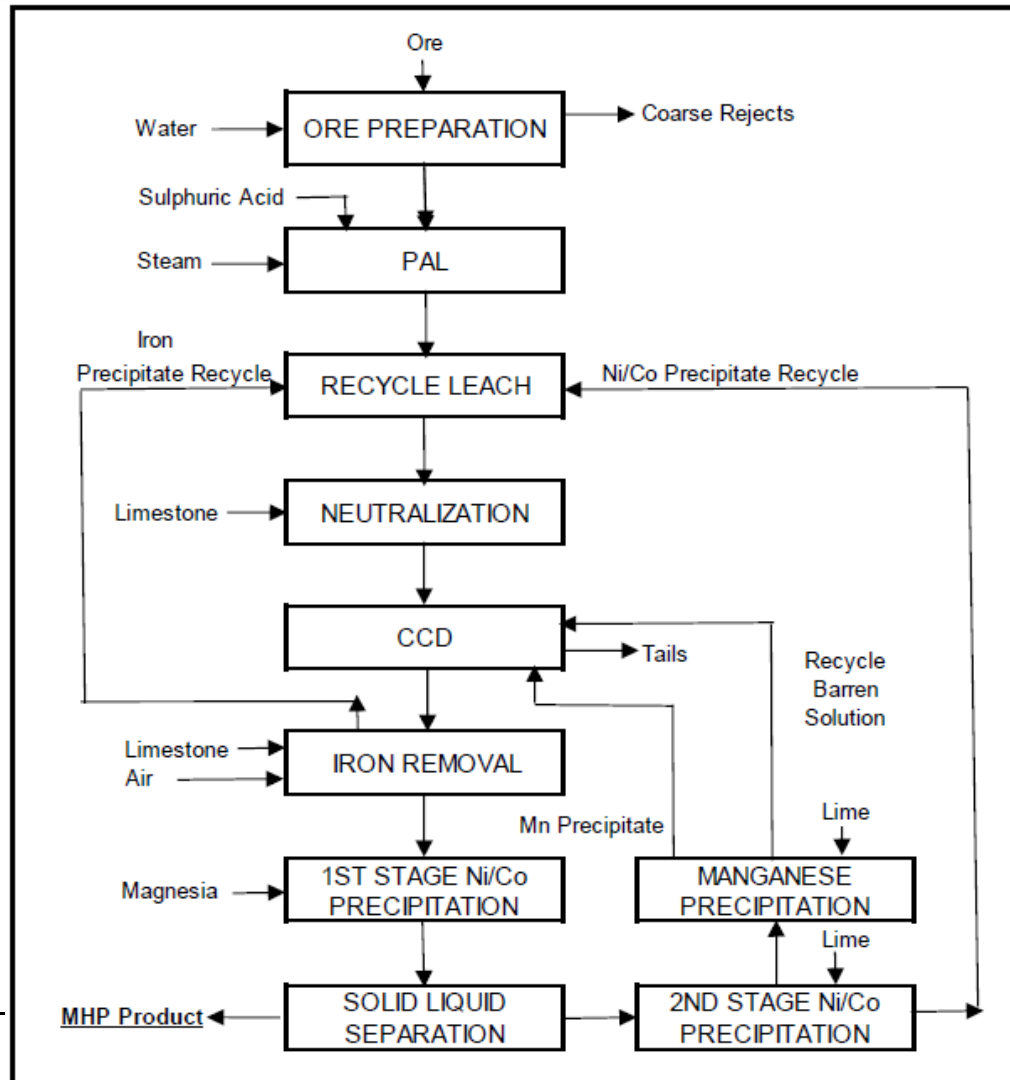


- A sulphide ore can usually easily be upgraded in Ni-concentration through a combination of comminution methods, like
  - Grinding
  - Milling
  - Classification
  - Flotation
  - Magnetic separation
  - And similar methods
- Ni-sulphide ores usually contain between 0.5 – 3% Ni
- “Ni-concentrates” (from upgrading) normally contain between 5 – 20% Ni
- An concentration ratio of 5-10 times is obtained.
- Not so with lateritic nickel ores, particularly the limonite type
- Typical grades in commercial mining operations:
  - Limonite: 1.0 - 1.7% Ni
  - Saprolite: 1.5 - 3% Ni



# HPAL principal flowsheet for Limonite ores

## Front end (up to intermediate/concentrate)



### Intermediate options:

#### MSP:

- Mixed Sulphide Precipitation
- Use  $H_2S(g)$ , low pressure

#### MHP:

- Mixed Hydroxide Precipitation
- Use "activated"  $MgO$

#### Direct SX:

- One example - Cyanex301
- Other example – DEHPA+Versatic10 (not in oper.)

# HPAL Flowsheet, Main chemistry

## Acid leaching



- Solubilize Ni and Co
- Keep Fe, Al (and some other elements) in residue
- Reach low free acid concentration in solution

Ni and Co:

- $\text{MeO} + \text{H}_2\text{SO}_4 = \text{MeSO}_4 + \text{H}_2\text{O}$ , Me = Ni, Co

Fe:

- Step 1:  $2\text{FeO}(\text{OH}) + 3\text{H}_2\text{SO}_4 = \text{Fe}_2(\text{SO}_4)_3 + 4\text{H}_2\text{O}$
- Step 2:  $2\text{Fe}(\text{SO}_4)_3 + 3\text{H}_2\text{O} = \text{Fe}_2\text{O}_3 + 3\text{H}_2\text{SO}_4$
- Net:  $2\text{FeO}(\text{OH}) = \text{Fe}_2\text{O}_3 + \text{H}_2\text{O}$
- Fe may also form some  $\text{Fe}_x\text{O}_y(\text{SO}_4)_z$ , basic sulphates

# HPAL Flowsheet, Main chemistry

## Intermediate precipitation



- Remove dissolved Ni and Co from pregnant leach solution
- In a form acceptable to a refinery
  - Both chemically (like impurity content) and physically

Mixed Sulphide Precipitation (MSP):

- $\text{MeSO}_4 + \text{H}_2\text{S(g)} = \text{MeS(s)} + \text{H}_2\text{SO}_4$ , Me = Ni, Co, others

Mixed Hydroxide Precipitation (MHP):

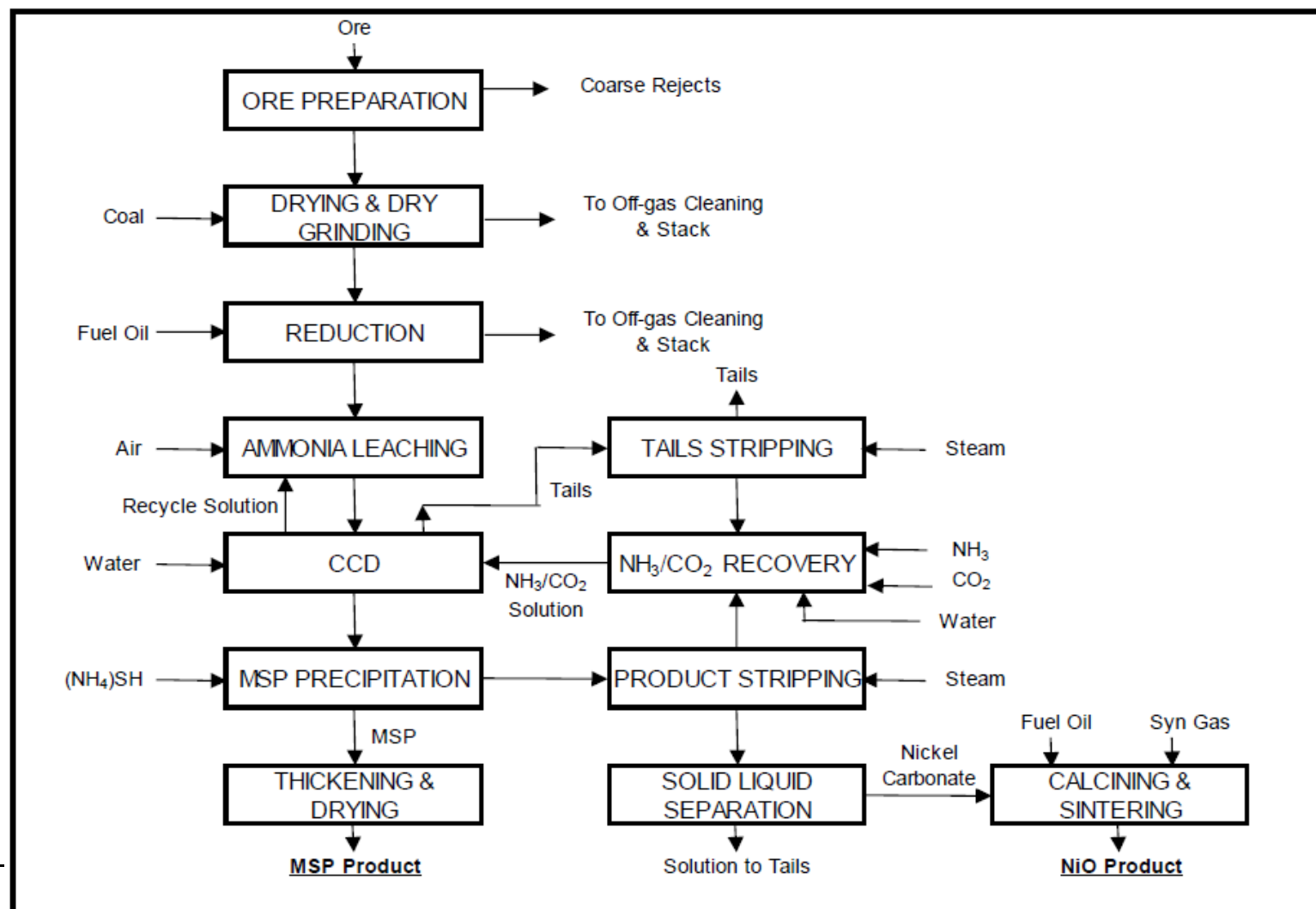
- $\text{MeSO}_4 + \text{MgO(s)} = \text{Me(OH)}_2\text{(s)} + \text{MgSO}_4$ , Me = Ni, Co, others

Comments:

- MSP:
  - Technically more challenging
  - Better acceptance of MSP vs. MHP, can easily be fed into Ni-matte refineries



# Caron principal flowsheet for Limonite ores



# Caron Flowsheet, Main chemistry

## 1. Reducing roast

- Selectively metallize Ni and Co
  - Partial reduction of iron to magnetite
  - A small amount of iron is also metallized
  - Metallic phase is a Ni-Fe-Co alloy, Ni/Fe ratio  $\approx \frac{1}{2}$
- 
- $3 \text{Fe}_2\text{O}_3 + \text{CO} = 2 \text{Fe}_3\text{O}_4 + \text{CO}_2$
  - $\text{NiO} + \text{CO} = \text{Ni} + \text{CO}_2$
  - $\text{Fe}_3\text{O}_4 + \text{CO} = 3 \text{Fe} + \text{CO}_2$
  - $\text{CoO} + \text{CO} = \text{Co} + \text{CO}_2$
  - $\text{Fe}_3\text{O}_4 + \text{CO} = \text{FeO} + \text{CO}_2$

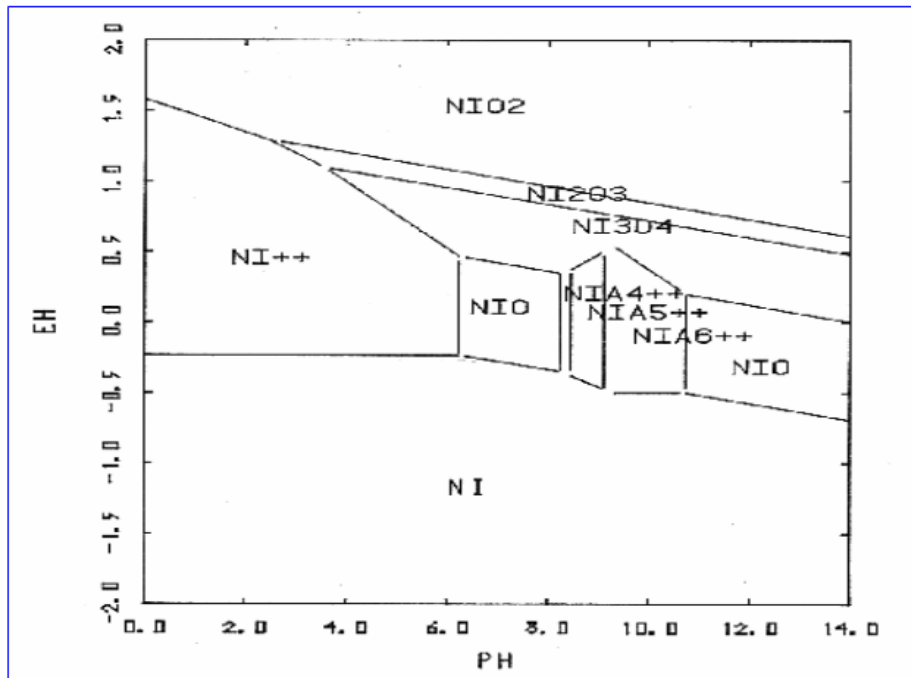


# Caron Flowsheet, Main chemistry

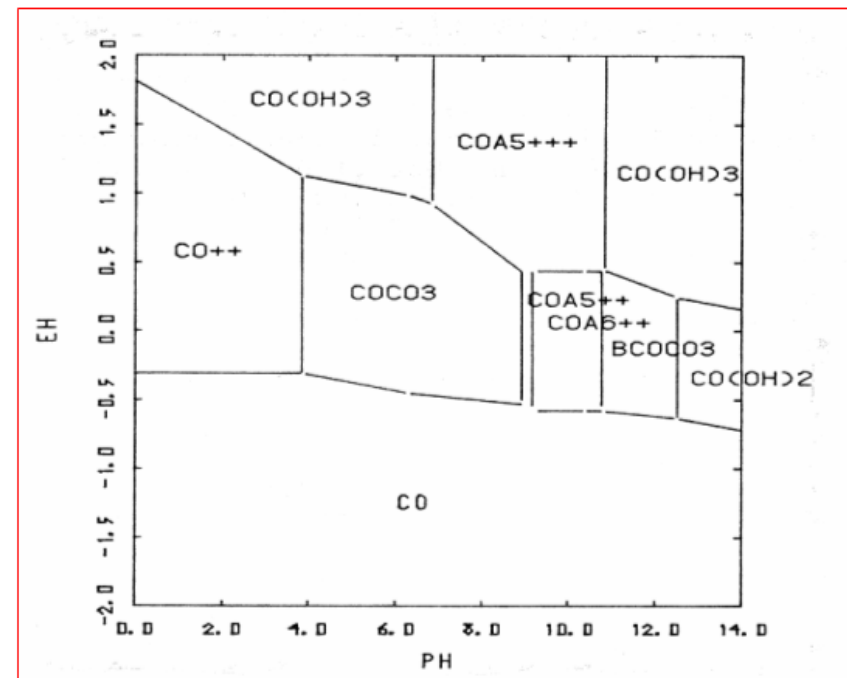
## Ni and Co solubility in NH<sub>3</sub>-solutions



Ni-NH<sub>3</sub>-H<sub>2</sub>O system: [Ni] = 1 M, [N] = 1M



Co-NH<sub>3</sub>-CO<sub>3</sub>-H<sub>2</sub>O System





# Caron Flowsheet, Main chemistry

## Oxidative leach and complex ion formation

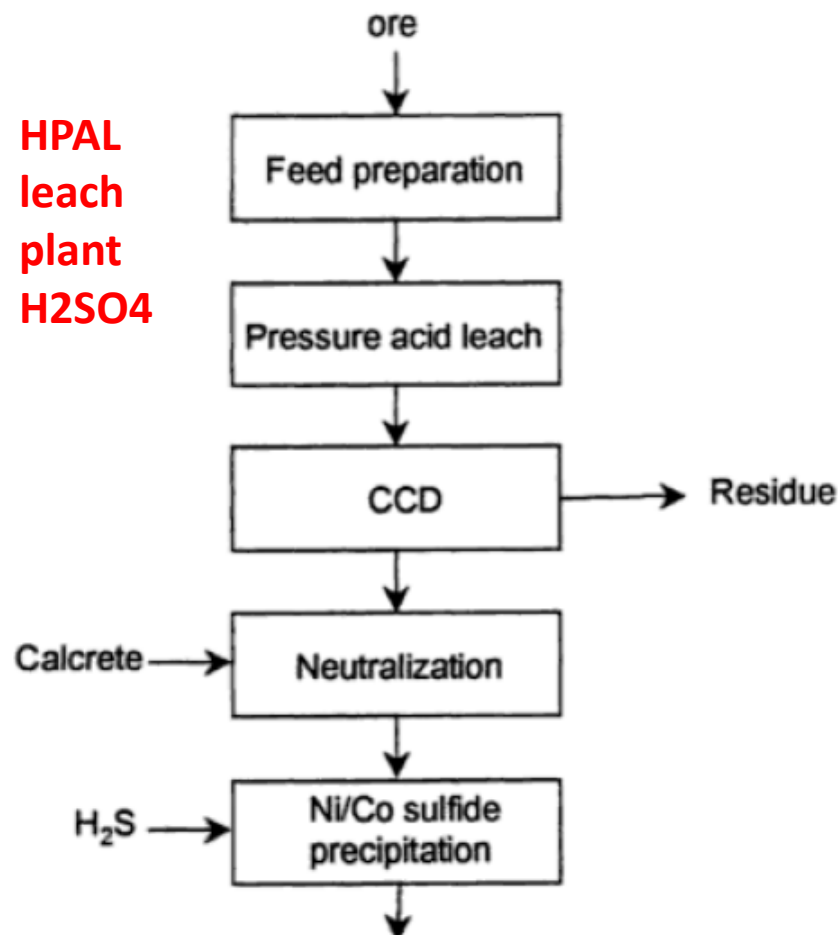


- Subreactions:
- $M = M^{2+} + 2 e^-$
- $M^{2+} + 6 NH_3 = M(NH_3)_6^{2+}$
- $Co(NH_3)_6^{2+} = Co(NH_3)_6^{3+} + e^-$
- Role of Oxygen:
  - $O_2 + 2 H_2O + 4 e^- = 4 OH^-$
- Buffersystem  $NH_3$ - $CO_2$ :
- $NH_3(g) + CO_2(g) + H_2O = (NH_4)_2CO_3 = 2NH_4^+ + CO_3^{2-}$ .
- 120 g/l  $NH_3$  + 100 g/l  $CO_2$  form ca. 2 M  $(NH_4)_2CO_3$  and 2.5-3 M "free"  $NH_3$ .
- Net leach reaction:
- $M(s) + \frac{1}{2} O_2(g) + 2 NH_4^+ + 4NH_3 = M(NH_3)_6^{2+} + H_2O$
- Salt i solution:  $M(NH_3)_6^{2+}$  (kation) +  $CO_3^{2-}$  (anion).

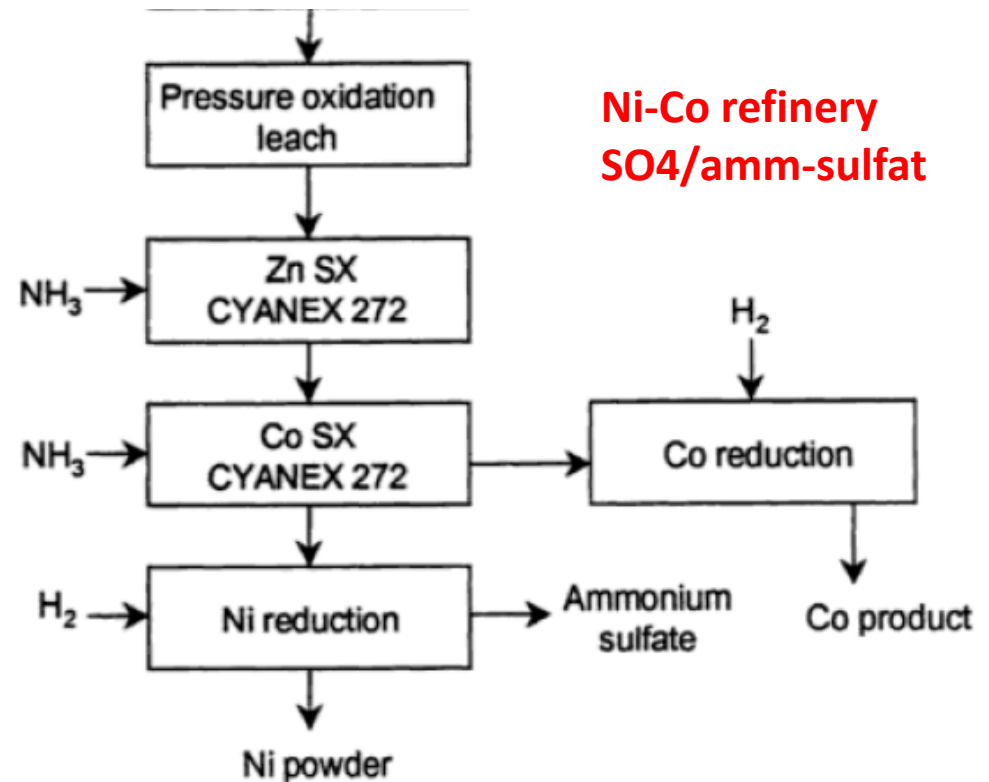
# Glencore "Murrin Murrin", W.Australia: 45 000 T/a Ni HPAL Laterite operations



**HPAL  
leach  
plant  
H<sub>2</sub>SO<sub>4</sub>**

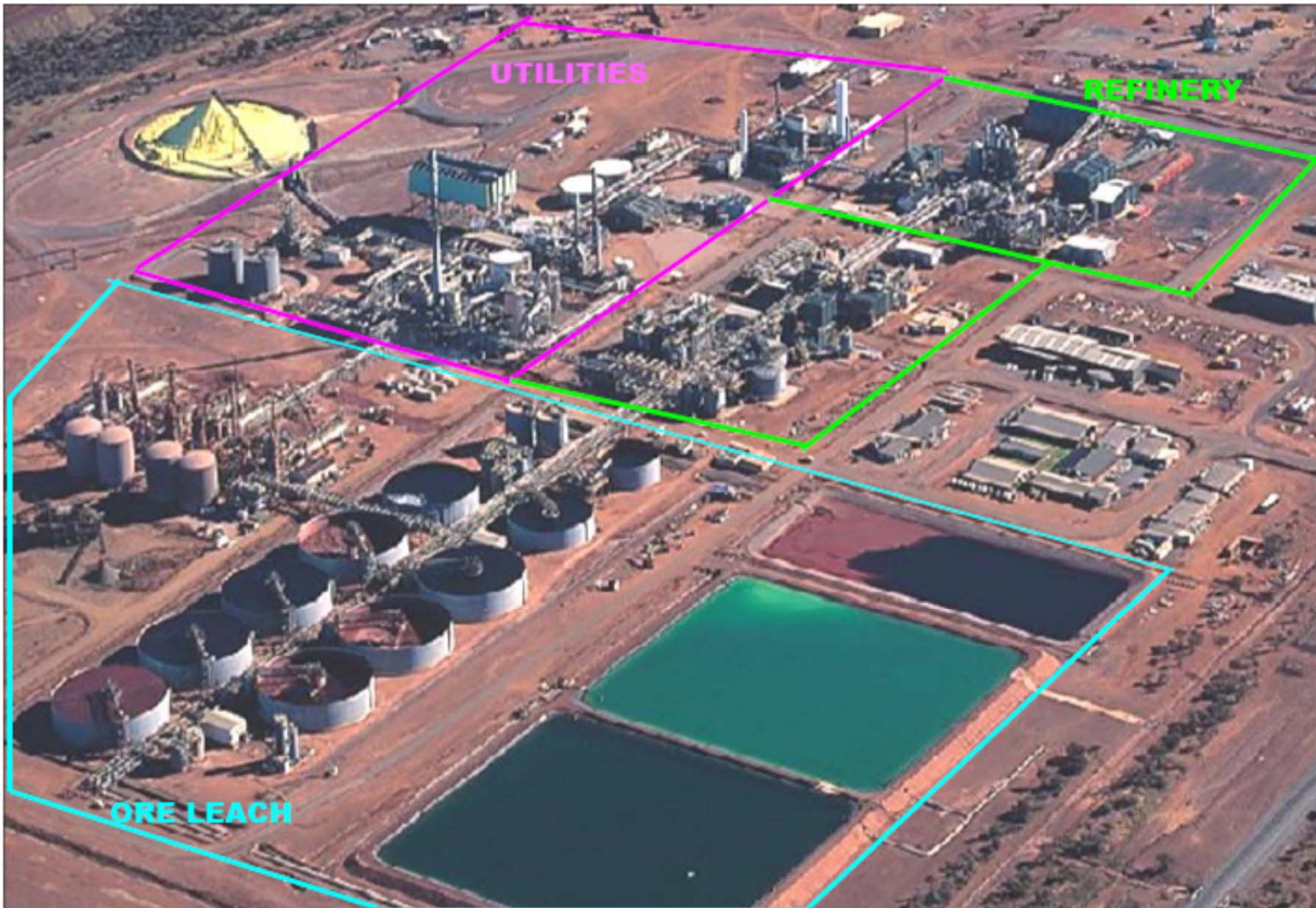


**Ni-Co refinery  
SO<sub>4</sub>/amm-sulfat**





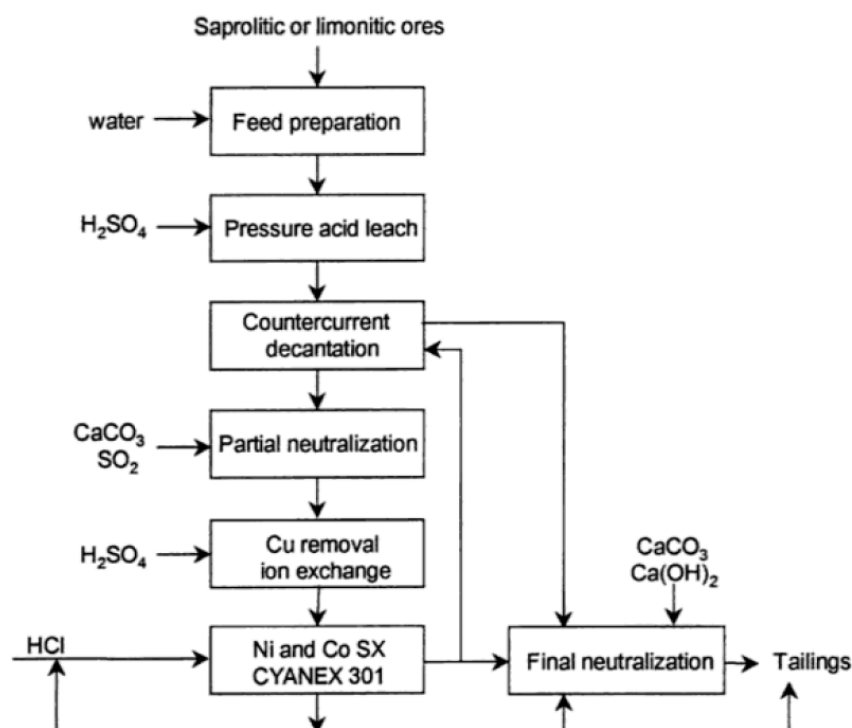
# Glencore "Murrin Murrin" operations, metallurgical site



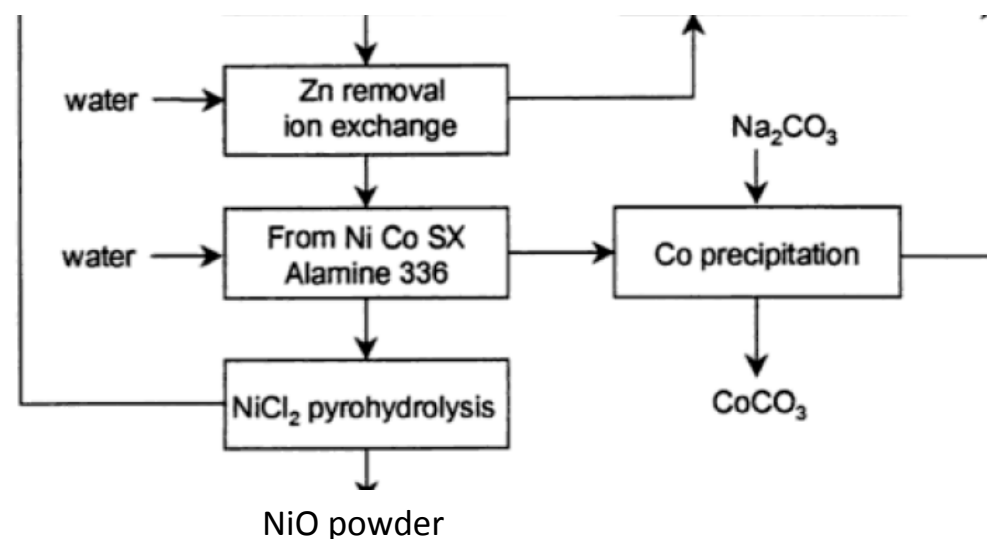
# VALE “Goro”, New Caledonia: 50 000 T/a Ni laterite HPAL with Cl-based refinery



## HPAL leach plant H<sub>2</sub>SO<sub>4</sub>



## Ni-Co refinery Cl/HCl





# VALE “Goro”, New Caledonia, metallurgical site



[illegible]

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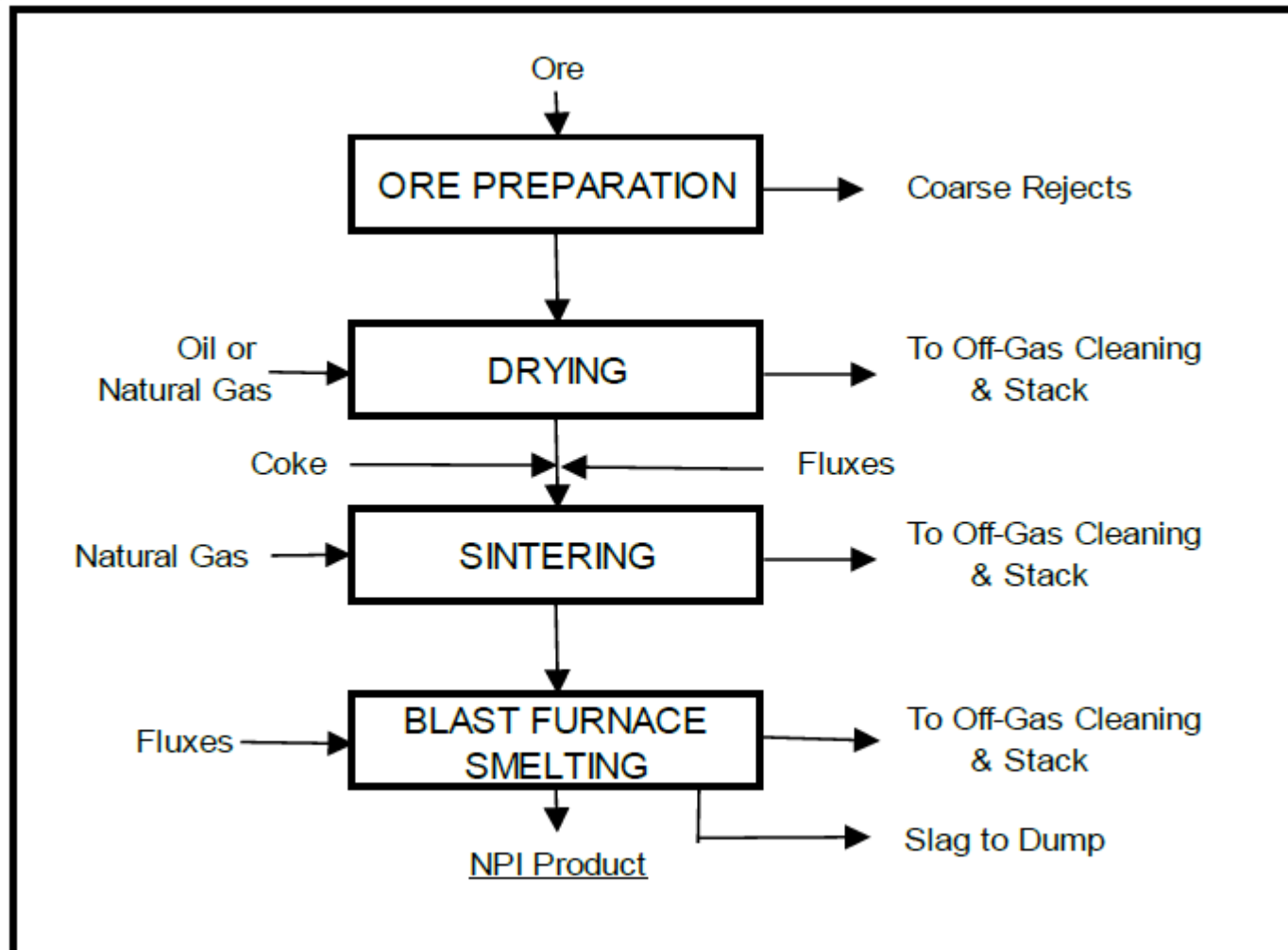


# Queensland Nickel operations, metallurgical site ca. mid-2000





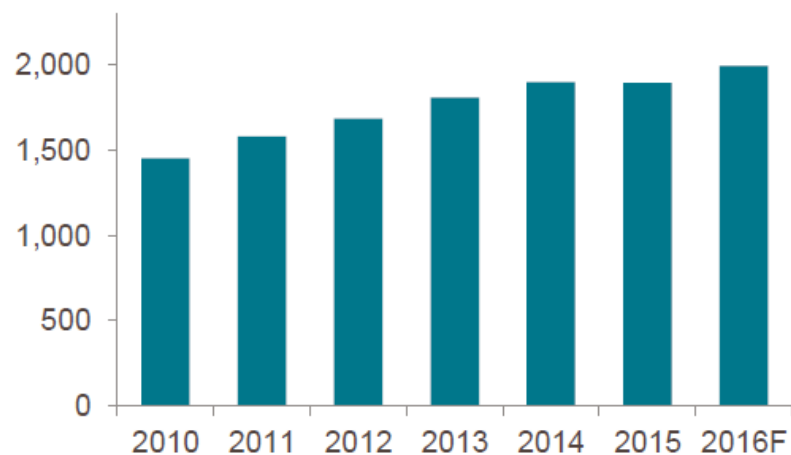
# Nickel Pig Iron (NPI) flowsheet, here with blast furnace.



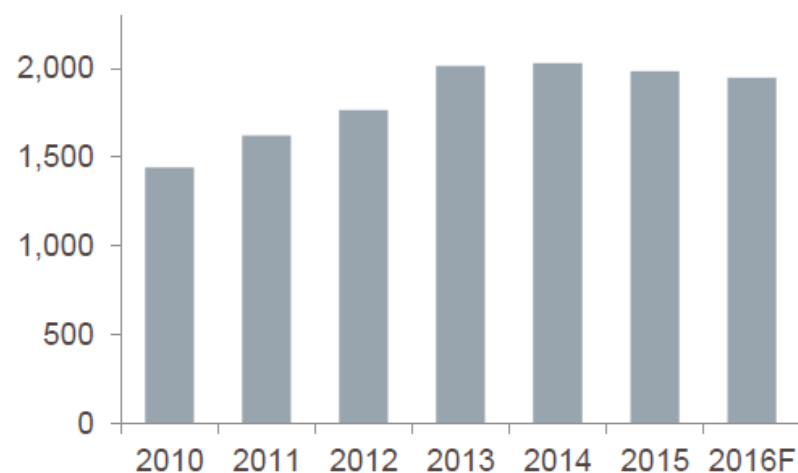
# Global nickel market and NPI's influence



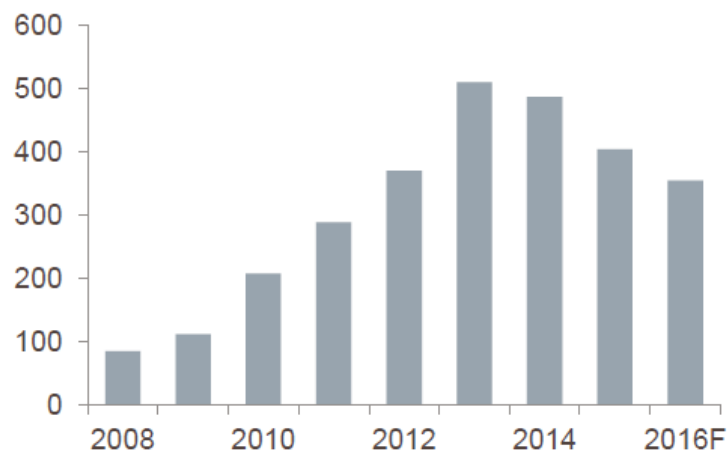
2010 – 2016 Primary nickel demand (kt Ni)



2010 – 2016 Global Nickel supply (kt Ni)



2008 – 2016 China NPI Output



2013 – 2020 Indonesian NPI supply (kt Ni)

